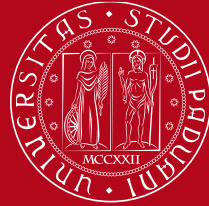


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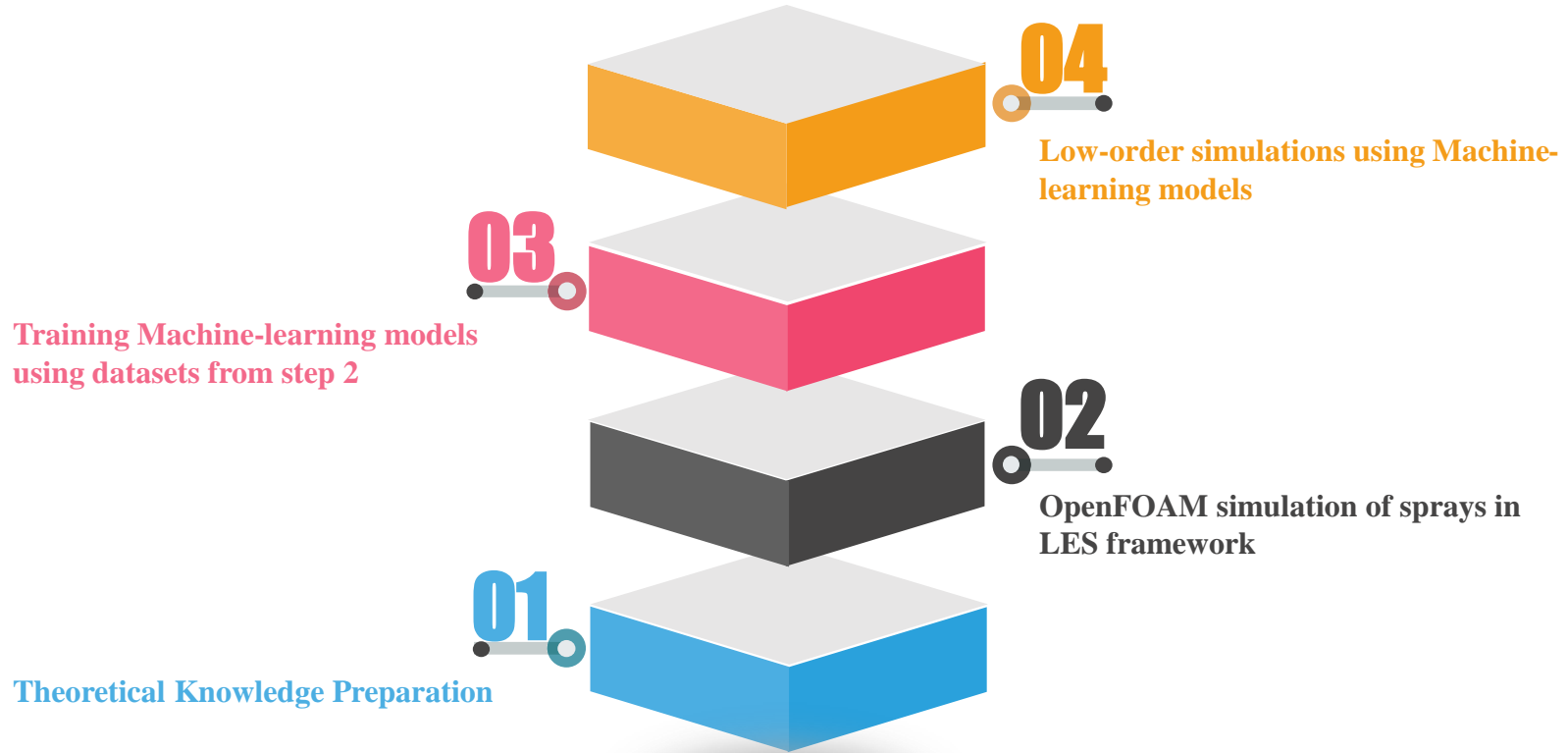
High-fidelity simulation and modeling of turbulent sprays

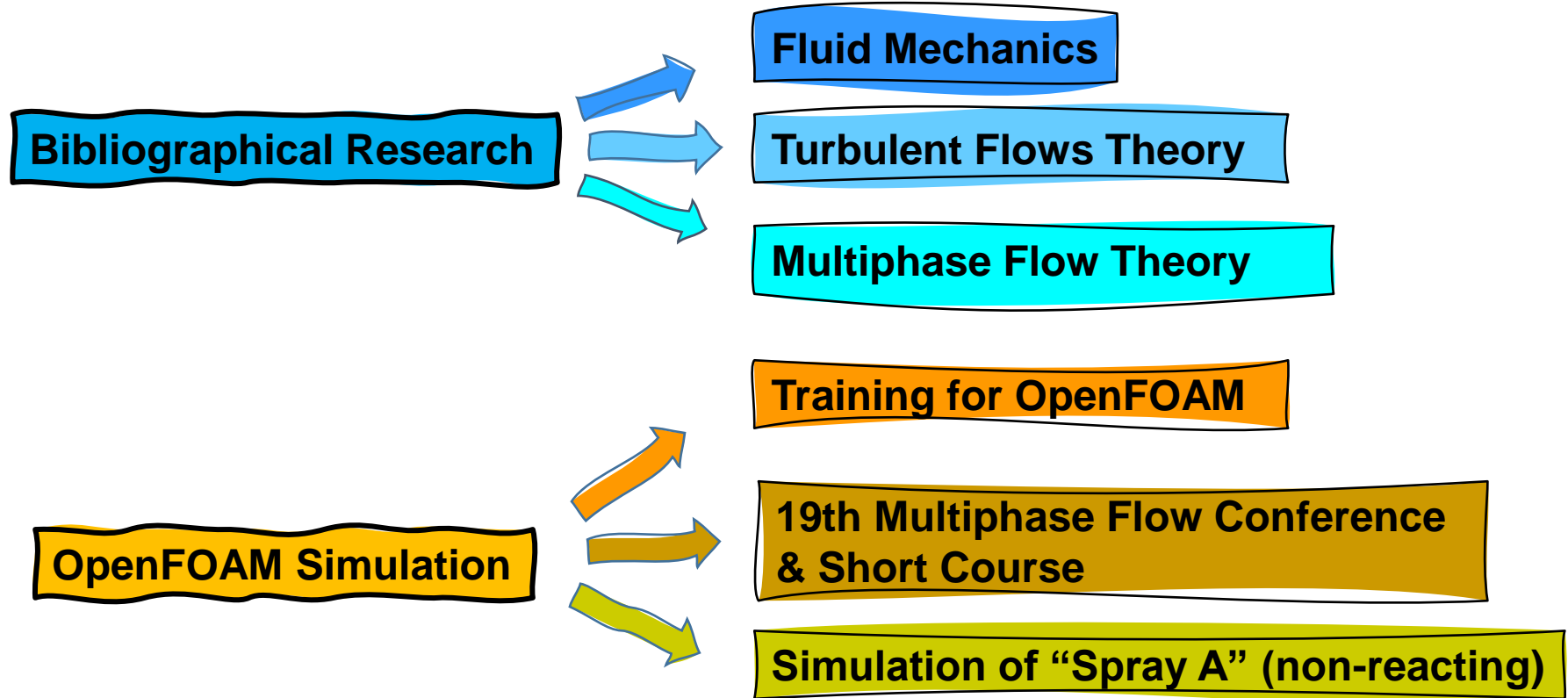
Xiang'en Kong - 38th Cycle

Supervisor: Prof. Francesco Picano

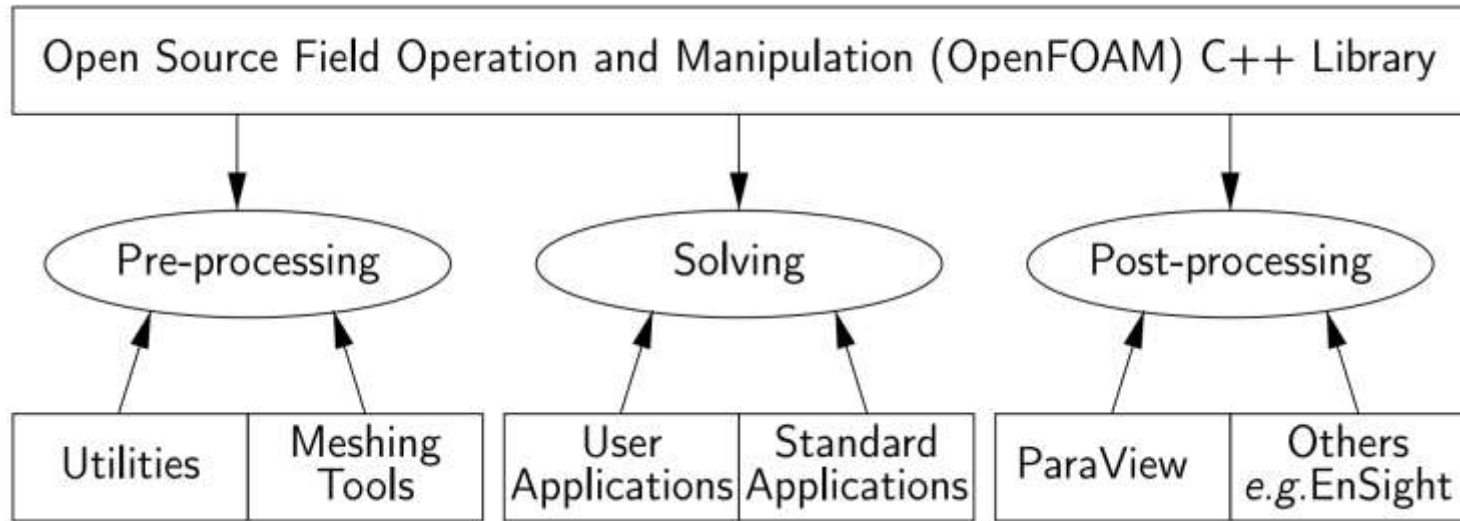
Co-supervisor: Dr. Federico Dalla Barba

Meeting - 13/09/2023





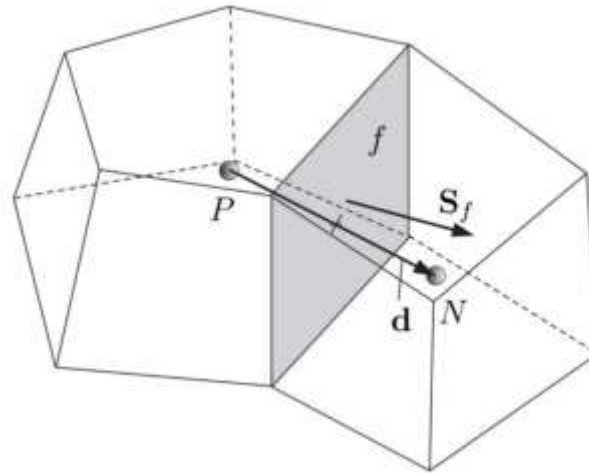
OpenFOAM (for "Open-source Field Operation And Manipulation") is a C++ toolbox for the development of customized numerical solvers, and pre-/post-processing utilities for the solution of continuum mechanics problems, most prominently including computational fluid dynamics (CFD).



OpenFOAM user's guide

Finite Volume Method (FVM)

A control volume is defined around every single grid point and the conservation laws must be respected if fluxes from any quantity are calculated through the interface between two different volumes. Due to this conservation property, FVM is more stable and hence chosen for solving CFD problems.



Details of discretised control volume (OpenFOAM user's guide)

High-fidelity simulation and modeling of turbulent sprays



sprayFoam is a transient PIMPLE solver for compressible, laminar or turbulent flows with a spray particle cloud.

sprayFoam uses Eulerian-Lagrangian approach and the interaction between the continuous phase and discrete phase is given by two-way coupling.

Eulerian Phase (LES)

Mass equation	{	$\frac{\partial \bar{\rho}}{\partial t} + \nabla \cdot (\bar{\rho} \tilde{\mathbf{v}}) = \bar{\rho}_l$
Momentum equation		$\frac{\partial \bar{\rho} \tilde{\mathbf{v}}}{\partial t} + \nabla \cdot (\bar{\rho} \tilde{\mathbf{v}} \otimes \tilde{\mathbf{v}}) = -\nabla \bar{p} + \nabla \cdot \bar{\boldsymbol{\tau}} + \bar{\rho} \mathbf{g} + \bar{\mathbf{f}}_l - \nabla \cdot \mathbf{B}$
Energy equation		$\frac{\partial \bar{\rho} \tilde{H}_K}{\partial t} + \nabla \cdot (\bar{\rho} \tilde{H}_K \tilde{\mathbf{v}}) = \frac{\partial \bar{p}}{\partial t} + W + \nabla \cdot (\bar{\alpha} \nabla \tilde{h}) + \bar{q}_c + \bar{q}_l - \nabla \cdot \mathbf{b}_E$
Mass fraction equation		$\frac{\partial \bar{\rho} \tilde{Y}_i}{\partial t} + \nabla \cdot (\bar{\rho} \tilde{Y}_i \tilde{\mathbf{v}}) = \nabla \cdot (D_i \nabla \tilde{Y}_i) + \bar{\omega}_{ic} + \bar{m}_{il} - \nabla \cdot \mathbf{b}_i$

Lagrangian Phase

Mass equation

$$\frac{dm_d}{dt} = \frac{m_d}{\tau_i}$$

Momentum equation

$$m_d \frac{du_d}{dt} = -\frac{\pi D^2}{8} \rho C_d |u_d - u| (u_d - u) + F_G + F_P$$

Energy equation

$$m_d \frac{dh_d}{dt} = \dot{m}_d h_v(T_d) + \pi D \cdot k_v \cdot Nu \cdot (T - T_d) f$$

Lagrangian Phase

Particle Forces

Drag force
$$F_D = C_D \frac{\pi D_p^2}{8} \rho_f (u_f - u_p) |u_f - u_p|$$

where

- Schiller-Naumann (1935)

$$C_D = \begin{cases} \frac{24}{Re_p} (1 + 0.15 Re_p^{0.687}) & \text{if } Re_p \leq 1000 \\ 0.44 & \text{if } Re_p > 1000 \end{cases}$$

- Putnam (1961)

$$C_D = \begin{cases} \frac{24}{Re_p} (1 + \frac{1}{6} Re_p^{2/3}) & \text{if } Re_p \leq 1000 \\ 0.424 & \text{if } Re_p > 1000 \end{cases}$$

Lagrangian Phase

Gravity/Buoyancy force

$$F_G = m_p g \left(1 - \frac{\rho_f}{\rho_p} \right)$$

Pressure gradient force

$$F_P = -\frac{\pi D_p^3}{6} \nabla p$$

Other forces:

Added mass force

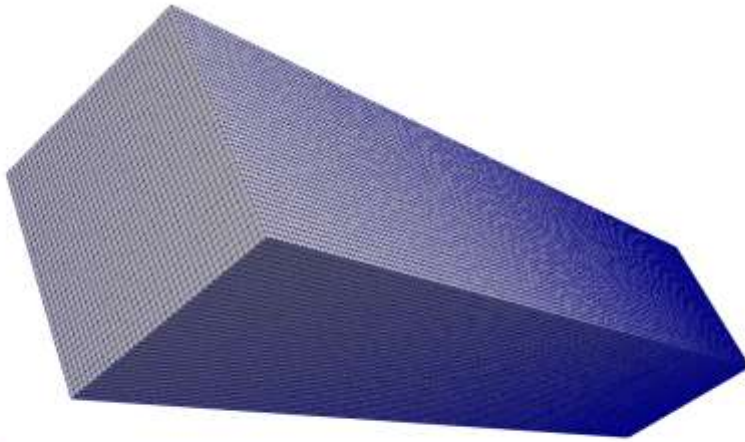
Thermophoretic force

Slip-rotation lift force

Slip-shear lift force

ECN (Engine Combustion Network) refers to the spray of n-dodecane as Spray A

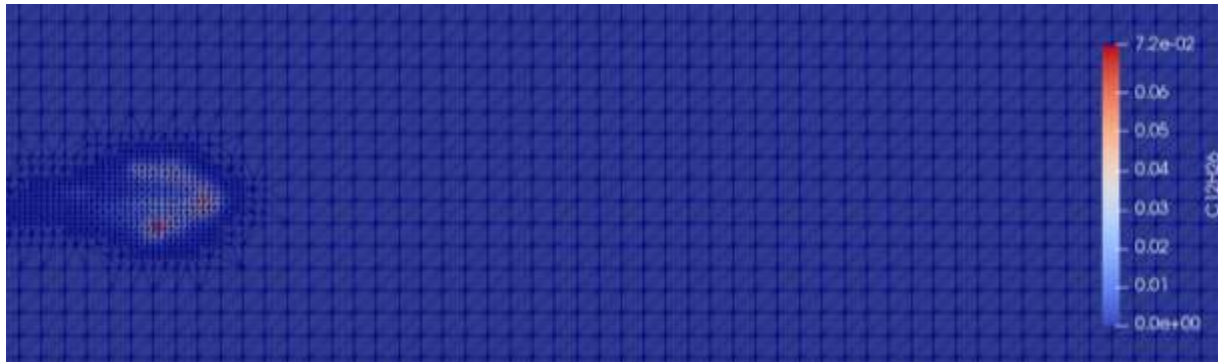
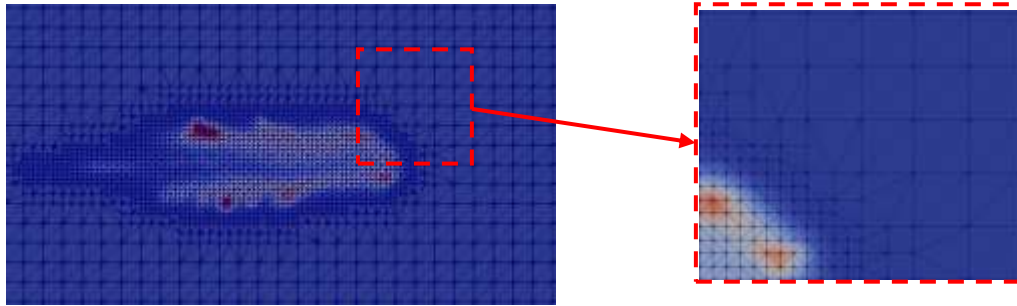
Specifications for Spray A operating condition of the Engine Combustion Network		Combustion chamber gas composition (volume fraction)		
Ambient gas temperature/K	900		Non-reacting	Reacting
Ambient gas pressure/MPa	Near 6.0	$\psi(\text{O}_2)$ / %	0	15
Ambient gas density/ kg/m ³	22.8	$\psi(\text{N}_2)$ / %	89.71	75
Ambient gas oxygen (by volume)/ %	15 (reacting); 0 (non-reacting).	$\psi(\text{H}_2\text{O})$ / %	6.52	6.38
Fuel injector nominal nozzle outlet diameter/mm	0.090	$\psi(\text{CO}_2)$ / %	3.77	3.62
Nozzle K factor	1.5			
Number of holes	1			
Orifice orientation	Axial			
Fuel injection pressure/ Mpa	50			
n-dodecane density/ kg/m ³	698			
Fuel temperature at nozzle /K	363			
Injection duration / ms	1.5			
Injection mass / mg	1.92			



Length	Width	Height
20mm	20mm	100mm

	Case1	Case2
grids	320000	871808
Min size	0.125mm	0.09mm

Adaptive mesh refinement (AMR) is relevant for CFD since it can greatly reduce the computational effort needed to solve a lot of cases.



Cut plane of the 3-D computational domain and the illustration of AMR

Perssure-velocity coupling: PIMPLE algorithm

LES Model: one-equation eddy viscosity model (kEqn)

Injection Model:

Initial droplet distribution: RosinRammler

breakup Model: ReitzKHRT

Case1

C12H26

T

U

0.25ms



0.50ms



0.75ms

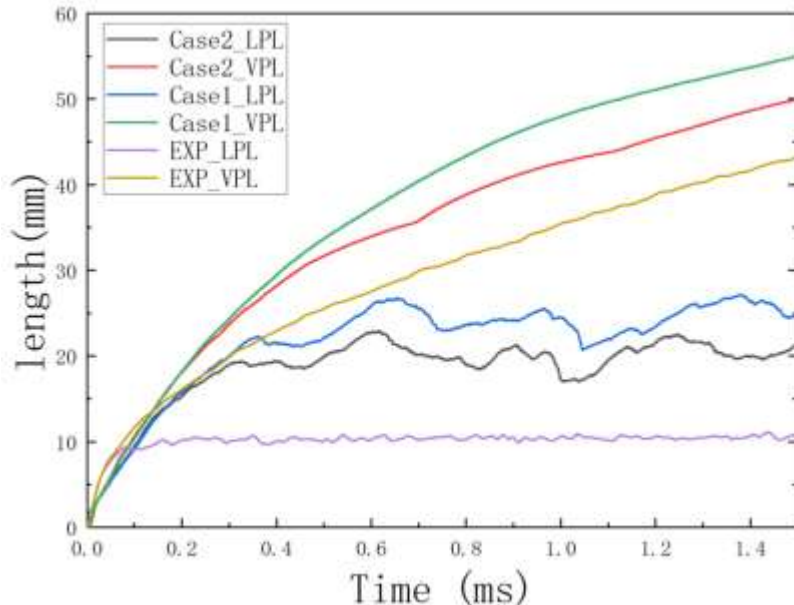


1.00ms



Liquid penetration length (LPL): the axial distance covering 95% of the injected liquid fuel mass

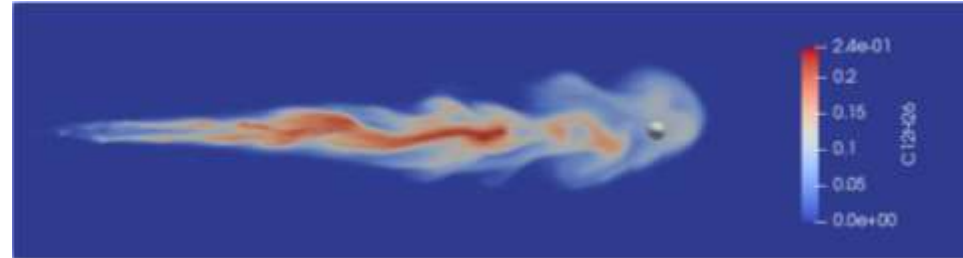
Vapour penetration length (VPL): distance from the nozzle tip to the location where the fuel mass fraction is 0.1% of its maximum value



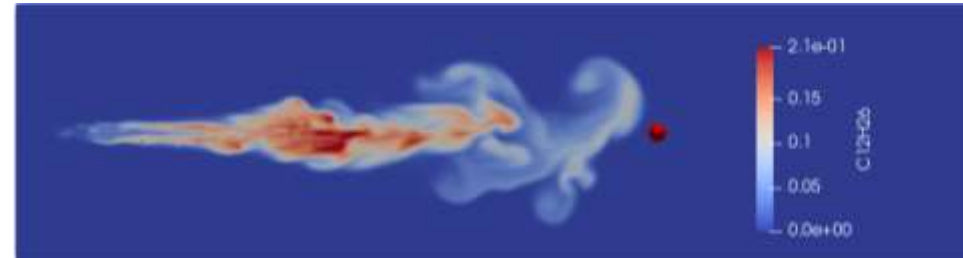
- Simulations have longer LPL and VPL than experiment
- Refining the mesh can shorten LPL and VPL
- It is necessary to adjust the parameters of the injection model to optimize the simulation results and make them more consistent with the experimental results

1.45 ms

Case1

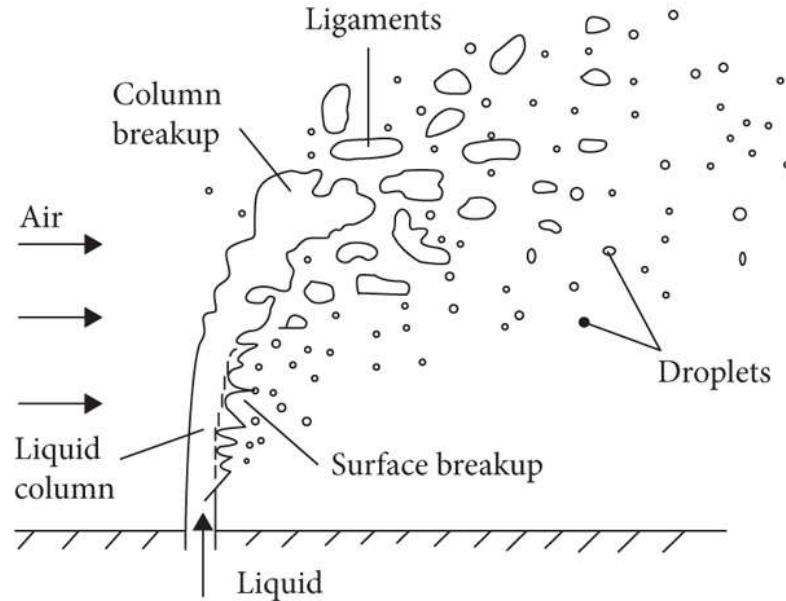


Case2



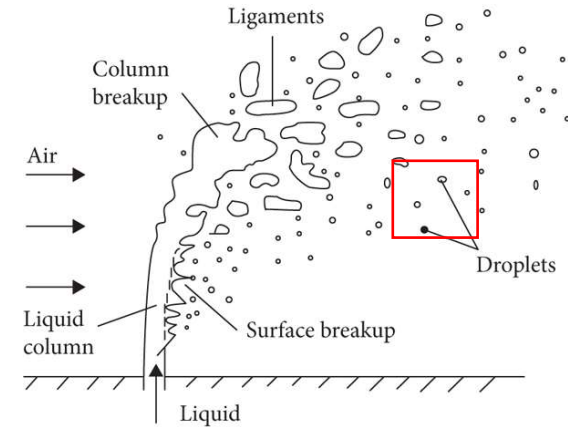
With decreasing the mesh size, the carrier gas radial dispersion increases

The following work will develop physics-based and AI-based model for spray dynamics considering dispersed droplet in a shear-layer



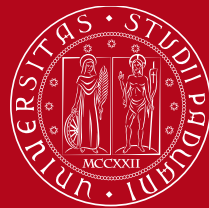
Droplet Size Spatial Distribution Model of Liquid Jets Injected into Crossflow

- **Different kinds of LES models will be applied in OpenFOAM to simulate the spray in crossflow**
- **Specific regions (Inside the red box) of the spray will be investigated for the dynamical behavior of the dispersed droplets**
- **The obtained data will then be used to train the AI model**



Thanks for the attention

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