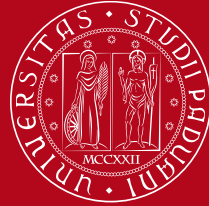


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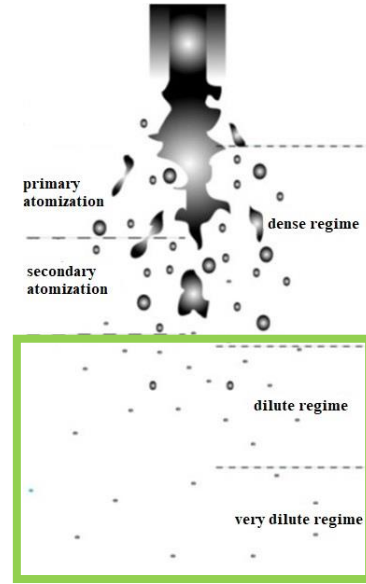
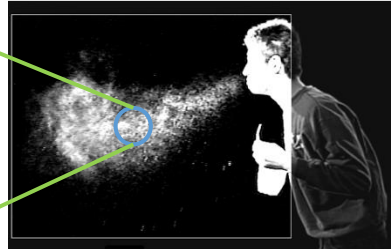
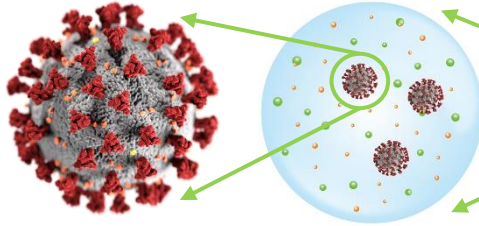
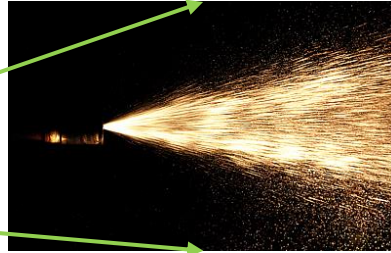
# Simulation And Modeling Turbulent Spray Dynamics

**Jietuo Wang - 34th Cycle**

**Supervisor: Prof./Dr. Francesco Picano**

**Admission to thesis evaluation - 15/12/2021**

❑ **Turbulent sprays** : Complex multiphase flows where two distinguished phases mutually interact exchanging mass, momentum and energy in a turbulent environment.



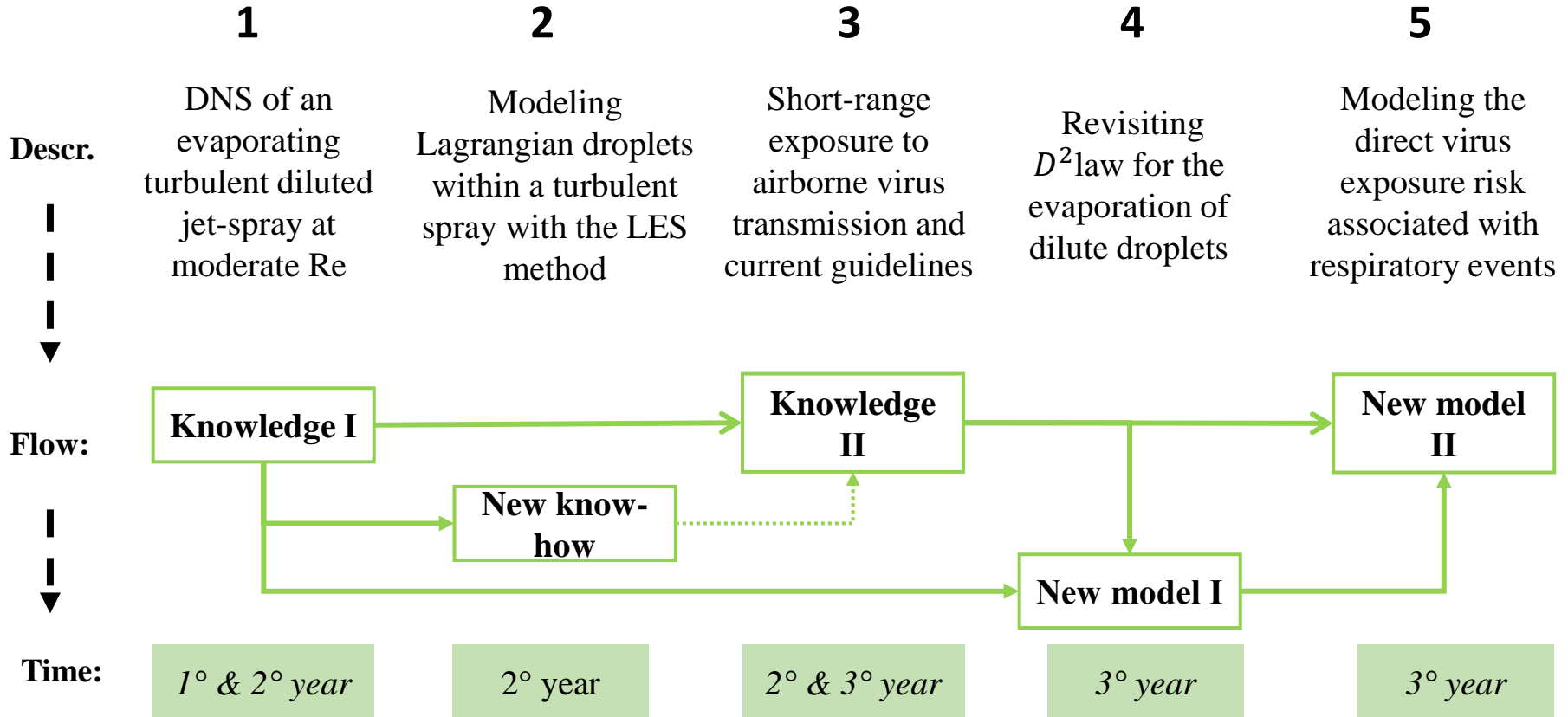
Sketch of various regimes in turbulent sprays [Jenny.2012]

## ❑ Diluted regime

- Dispersed droplets: **Point-droplet approximation**
- **No break-up** : surface tension  $\gg$  aerodynamic forces
- **low volume fraction** ( $\Phi < 10^{-3}$ ) : No collision / coalescence; **2-way coupling method**
- Main region occurring evaporation

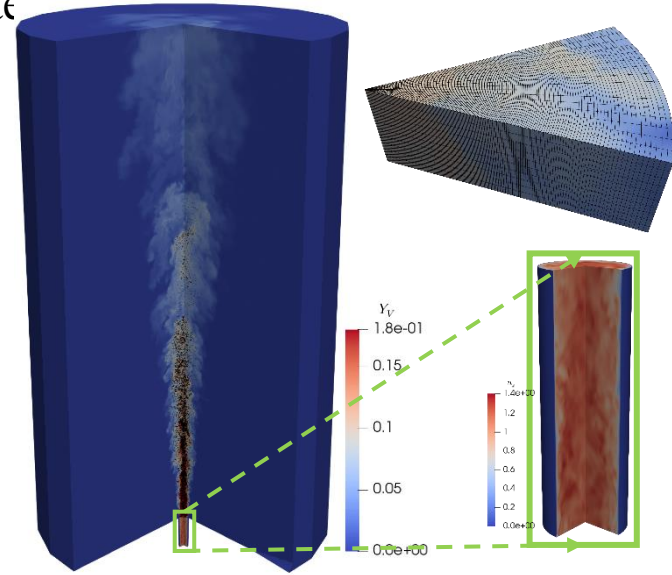
## ❑ Our goal

- Improve the current understanding of turbulent spray
- Apply our knowledge to solve practical issues
- Advance modeling capabilities related to turbulent spray



## □ Numerical Tool: CYCLONE

- Fully turbulent flow
- Staggered mesh
- Low Mach number NS & Point-droplet equations
- Cylindrical coordinate
- MPI parallelization



A sketch of the 3D cylindrical domain

## □ Formulations

**Eulerian Gas Phase**  
(Low Mach Navier- Stokes)

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{u}) = S_m$$

$$\frac{\partial}{\partial t} (\rho Y_V) + \nabla \cdot (\rho Y_V \mathbf{u}) = \nabla \cdot (\rho D \nabla Y_V) + S_m$$

$$\frac{\partial}{\partial t} (\rho \mathbf{u}) + \nabla \cdot (\rho \mathbf{u} \otimes \mathbf{u}) = \nabla \cdot \boldsymbol{\sigma} - \nabla P + S_p$$

$$\frac{\partial}{\partial t} (\rho E) + \nabla \cdot (\rho E \mathbf{u}) = -\nabla P \mathbf{u} + \nabla \cdot (\boldsymbol{\sigma} \otimes \mathbf{u}) - \nabla q + S_e$$

**Lagrangian dispersed phase**  
(Point-droplet equations)

$$\frac{d\mathbf{x}_d}{dt} = \mathbf{u}_d$$

$$\frac{d\mathbf{u}_d}{dt} = \frac{(\mathbf{u} - \mathbf{u}_d)}{\tau_d} (1 + 0.15 \text{Re}_d^{0.687})$$

$$\frac{dr_d^2}{dt} = -\frac{\mu_g \text{Sh}}{\rho_l \text{Sc}} \ln(1 + B_m)$$

$$\frac{dT_d}{dt} = \frac{\text{Nu}}{3\text{Pr}} \frac{c_{p,g}}{c_{p,l}} \frac{T - T_d}{\tau_d} + \frac{L_v}{c_{p,l}} \frac{\dot{m}_d}{m_d}$$

**2-way coupling terms**

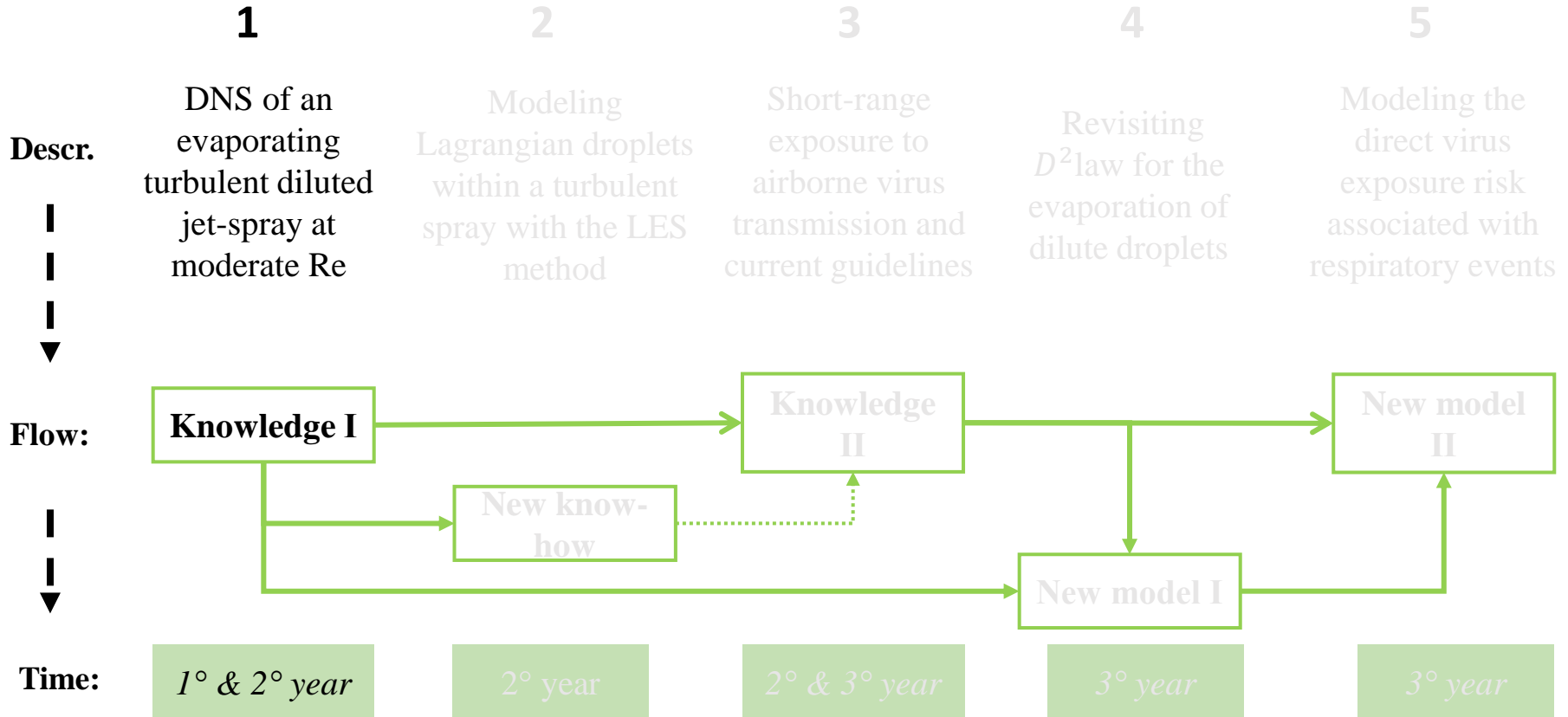
$$S_m = - \sum_{i=1} \frac{dm_{d,i}}{dt} \delta(\mathbf{x} - \mathbf{x}_{d,i})$$

$$S_e = - \sum_{i=1} \frac{d}{dt} (m_{d,i} c_{p,i} T_{d,i}) \delta(\mathbf{x} - \mathbf{x}_{d,i})$$

$$S_p = - \sum_{i=1} \frac{d}{dt} (m_{d,i} \mathbf{u}_{d,i}) \delta(\mathbf{x} - \mathbf{x}_{d,i})$$

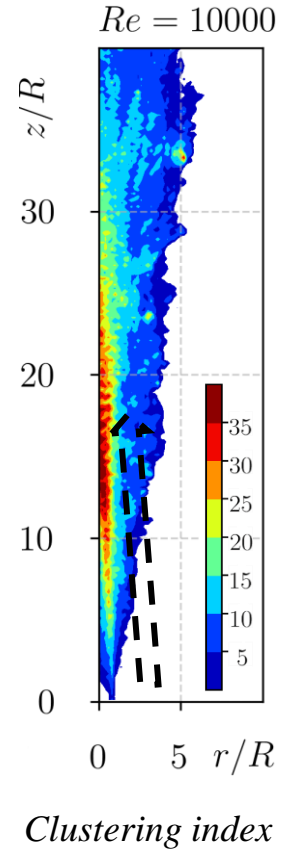
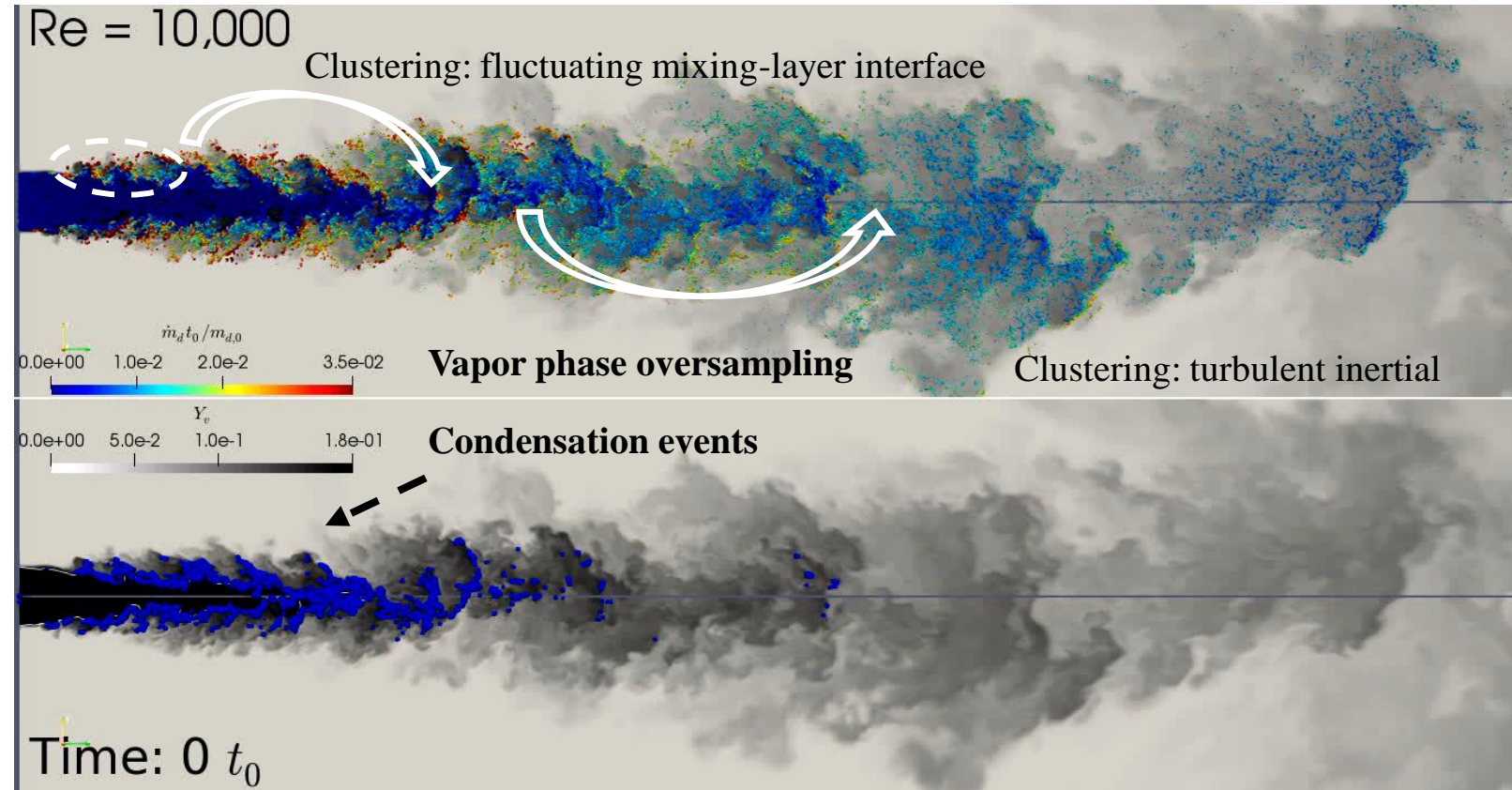
More details: Dalla Barba & Picano PRF 2018 and Wang et al. IJMF 2021

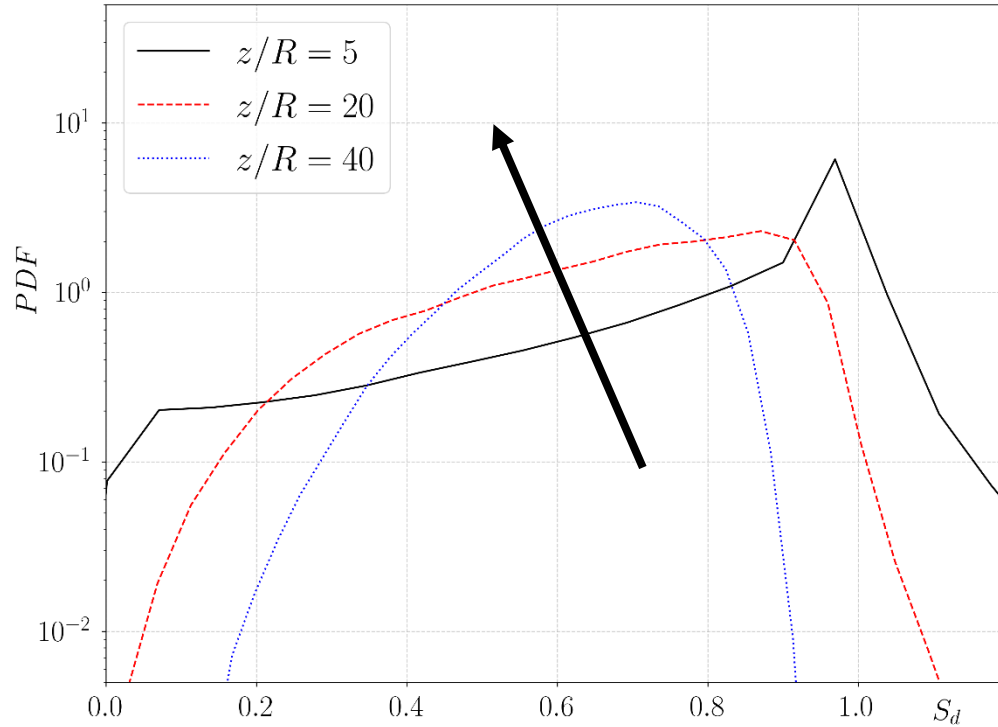
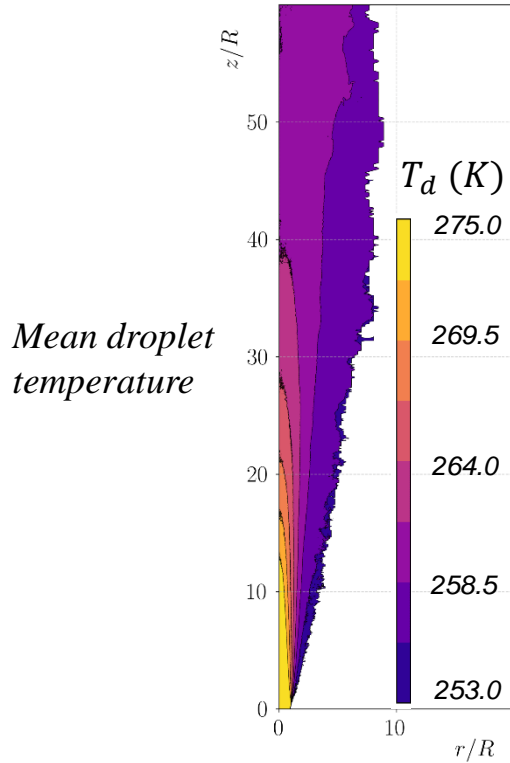
Modeling Turbulent Spray Dynamics



# Droplet evaporation: acetone spray

- Establishment and propagation of the preferential sampling of droplets





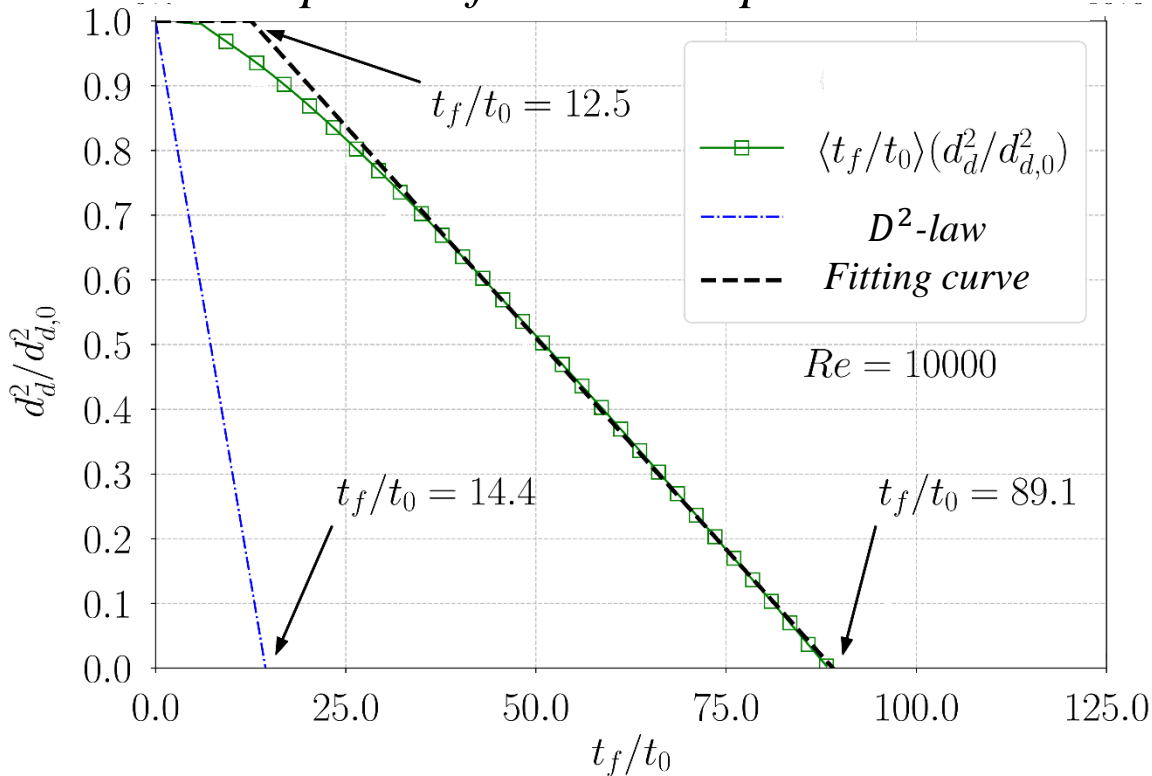
*PDF of the saturation field evaluated at the droplet surface*

- Lower droplet temperature w.r.t. initial value ( $\sim 20$  K)
- Wide distribution of saturation



- $\langle t_f \rangle (d_d^2/d_{d,0}^2)$ : Droplets mean flight time conditioned to the square droplet diameter

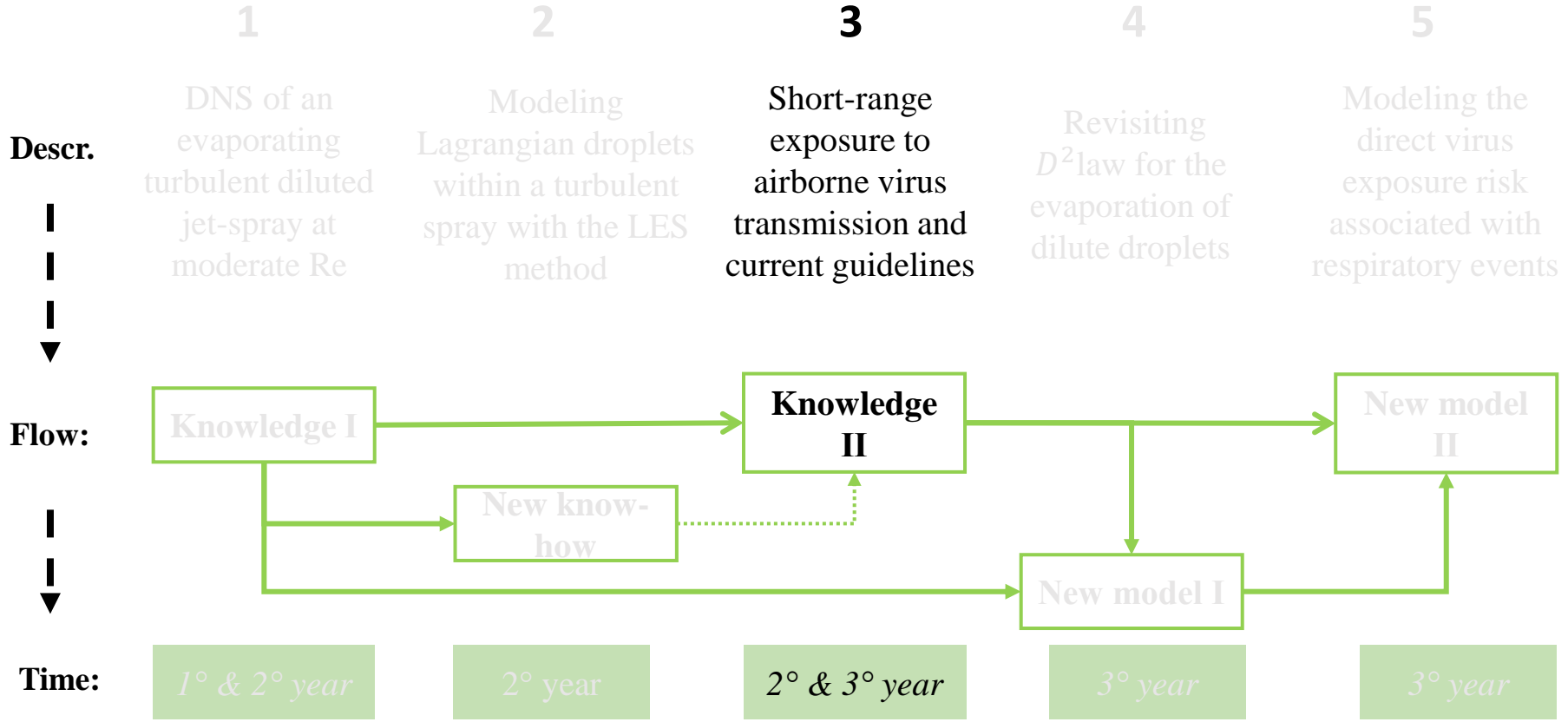
*Droplet surface v.s. evaporation time*



- $D^2$ -law is the classical and most used model for dilute evaporation: strongly underestimate droplet evaporation time.
- However, the mean droplet surface decreases in an almost linear trend, but with a small decay rate w.r.t. the classical model

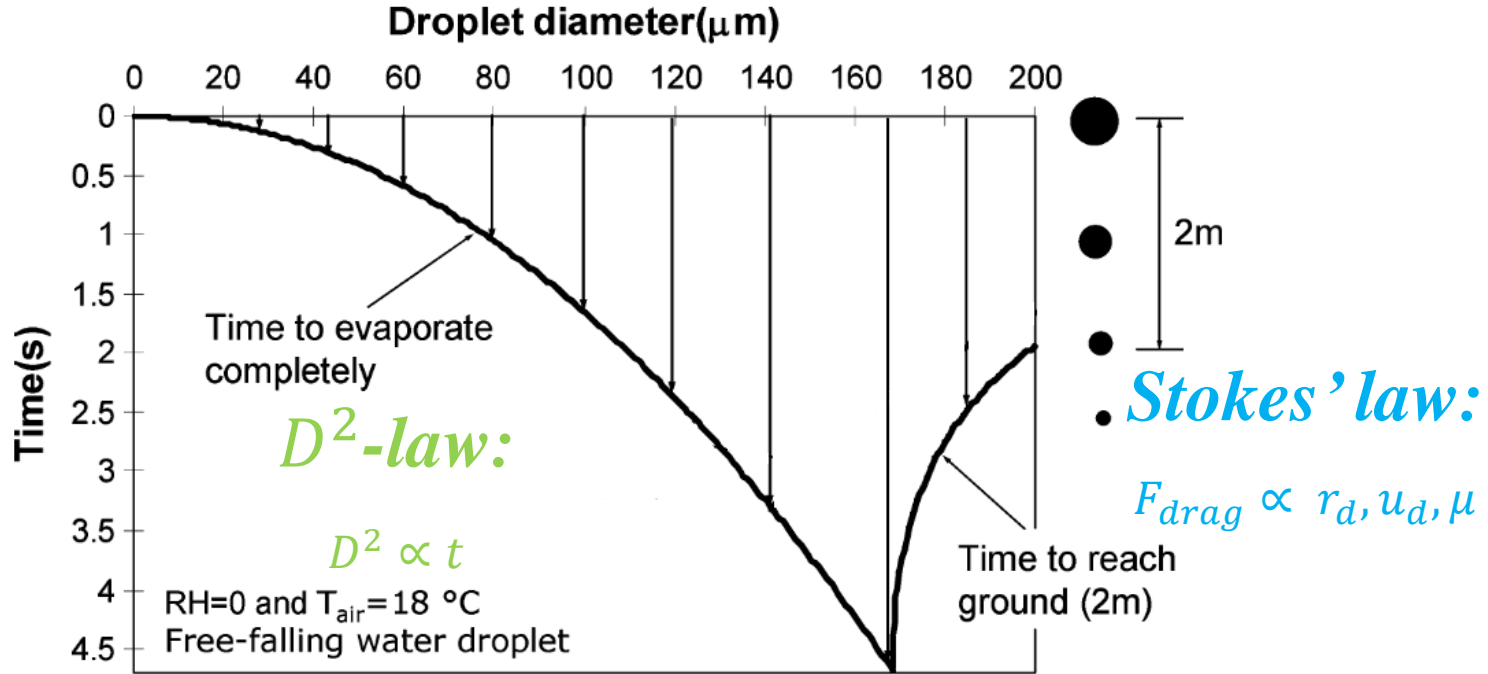
➔ Project 4





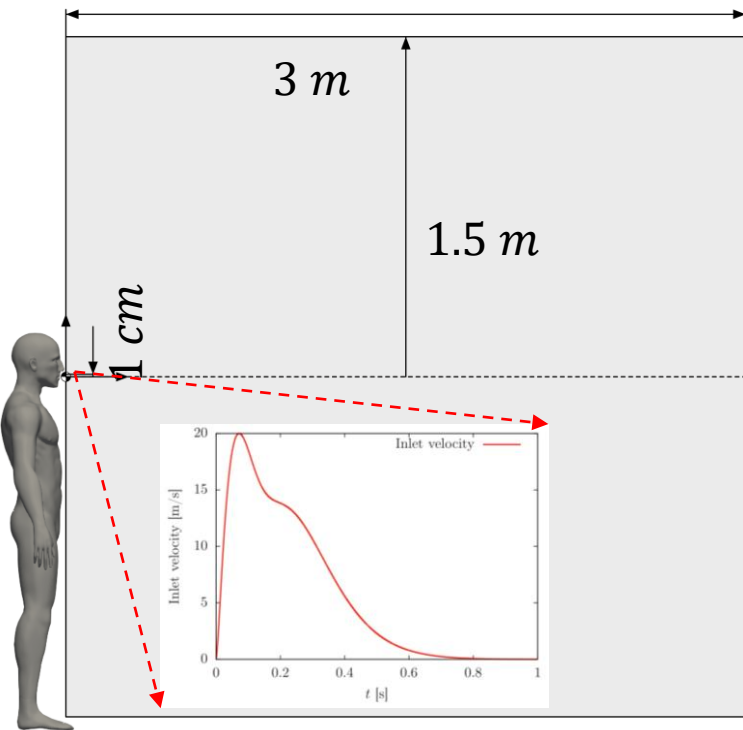
# Respiratory droplets: Wells theory

The Wells evaporation-falling curve of droplets



- This framework is so concise, readable and expressive that, since reported, it has been largely used in most public health guidelines, e.g. World Health Organization (WHO) and US Centers for Disease Control and Prevention (CDC).

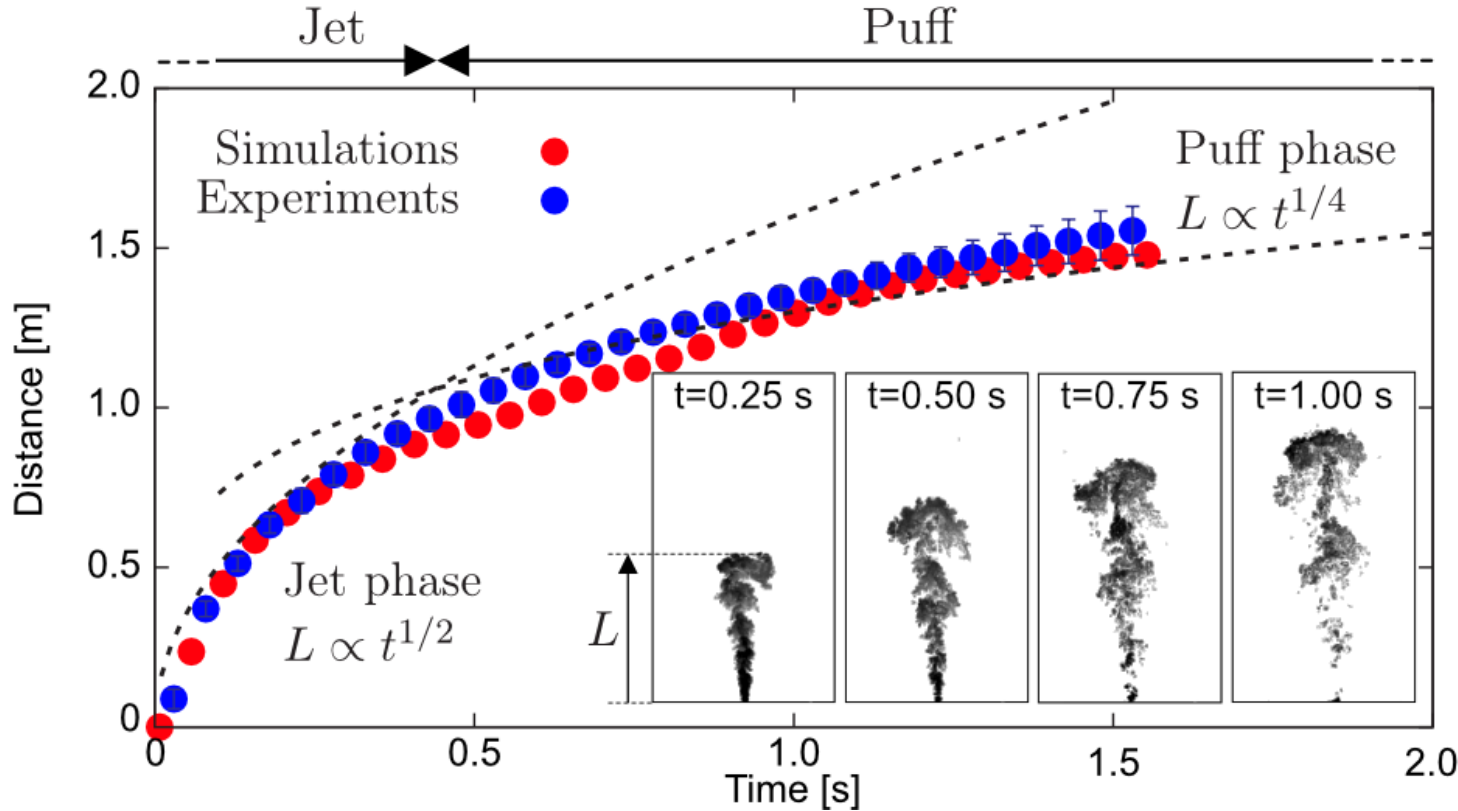
• Wells, W. F. (1934). *Am. J. Hyg.*, 20, 611-18. ; Xie, X., et al. (2007). *Indoor air*, 17(3), 211-225; Langmuir, I. (1918). *Phys. Rev.* 12, 368.



Up: sketch of the simulation setup used for the simulations;  
Right: summary of the simulation parameters and thermophysical properties

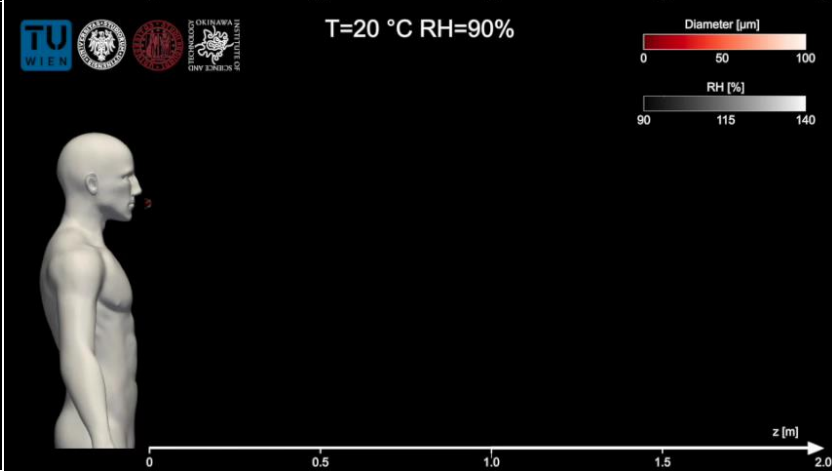
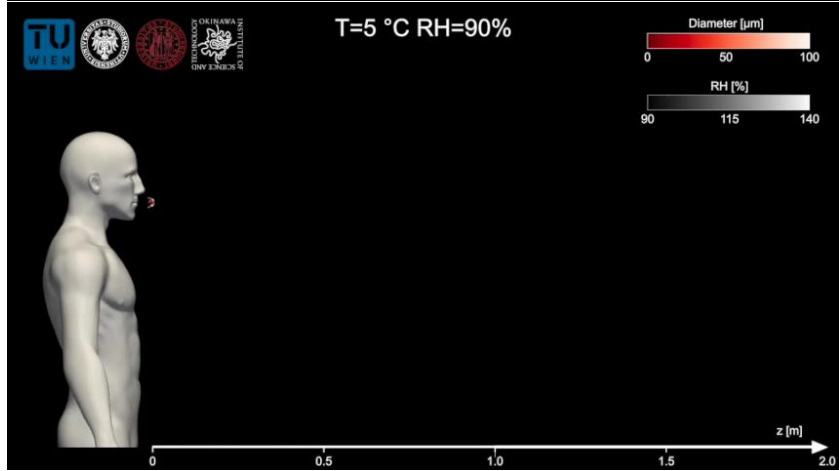
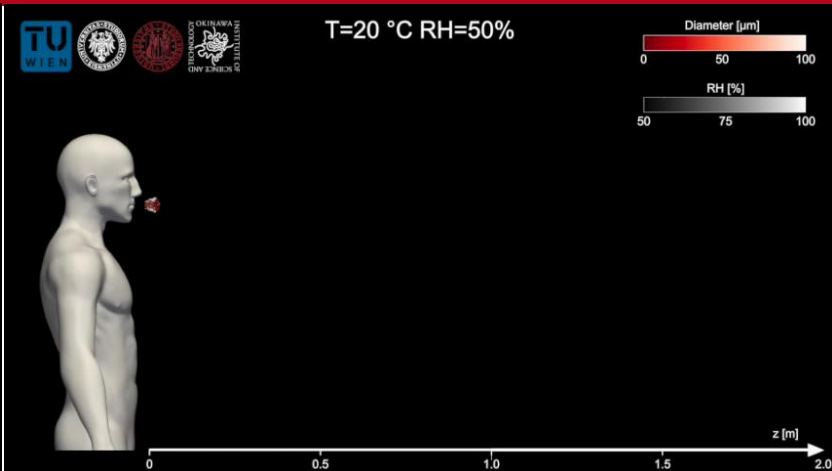
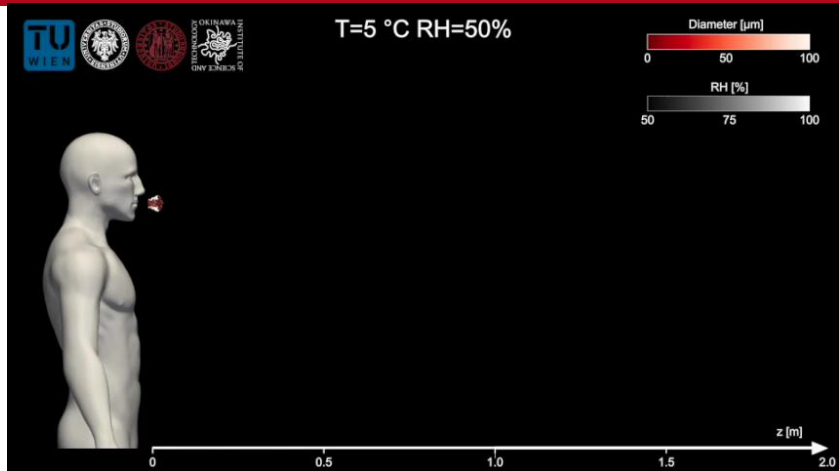
Parameter	Symbol	Value	Unit of measurement
Inlet radius	R	$1.00 \times 10^{-2}$	m
Sneezing jet temperature	$T_j$	308	K
Sneezing jet relative humidity	$RH_j$	90%	-
Maximum sneezing jet velocity	$u_{z,j}$	20	m/s
Droplets temperature	$T_k$	308	K
Mass injected liquid phase	$m_l$	$8.08 \times 10^{-6}$	kg
Mass injected gaseous phase	$m_g$	$2.00 \times 10^{-3}$	kg
Liquid mass fraction	$\Phi_m$	$4.04 \times 10^{-3}$	-
Liquid volume fraction	$\Phi_v$	$4.55 \times 10^{-6}$	-
Environment temperature	T	278 and 293	K
Environment relative humidity	RH	50% and 90%	-
Environment thermodynamic pressure	$p_0$	$1.01 \times 10^5$	Pa
Dynamic viscosity gaseous phase	$\mu_g$	$1.99 \times 10^{-5}$	Pa s
Thermal conductivity gaseous phase	$k_g$	$2.63 \times 10^{-2}$	W/(m*K)
Latent heat of vaporization	$L_v$	$2.41 \times 10^6$	J/kg
Universal gas constant	R	$2.87 \times 10^2$	J/(kg*K)
Molar mass of the gaseous phase	$W_g$	$2.89 \times 10^{-2}$	kg/mol
Gas constant gaseous phase	$R_g$	$2.92 \times 10^2$	J/(kg*K)
Specific heat capacity at constant pressure gaseous phase	$c_{p,g}$	$1.03 \times 10^3$	J/(kg*K)
Specific heat capacity at constant volume gaseous phase	$c_{v,g}$	$7.42 \times 10^2$	J/(kg*K)
Specific heat ratio gaseous phase	$\gamma$	1.39	-
Vapor specific heat capacity at constant pressure	$c_{p,v}$	$1.88 \times 10^3$	J/(kg*K)
Vapor phase gas constant	$R_v$	$4.61 \times 10^2$	J/(kg*K)
Binary mass diffusion coefficient	D	$2.67 \times 10^{-5}$	m <sup>2</sup> /s
Molar mass liquid phase	$W_l$	$1.80 \times 10^{-2}$	kg/mol
Density liquid phase	$\rho_l$	$1.00 \times 10^3$	kg/m <sup>3</sup>
Specific heat liquid phase	$c_l$	$4.18 \times 10^3$	J/(kg*K)
Volume fraction non-volatile material droplet	$\Phi_v^c$	3%	-
Prandtl number	$Pr$	0.782	-
Schmidt number	$Sc$	0.663	-

# Simulating sneeze: validation



*Distance traveled by the front of the jet: comparison between simulations and experiments. (Insets) Qualitative visualizations obtained from experiments showing the jet/puff evolution.*

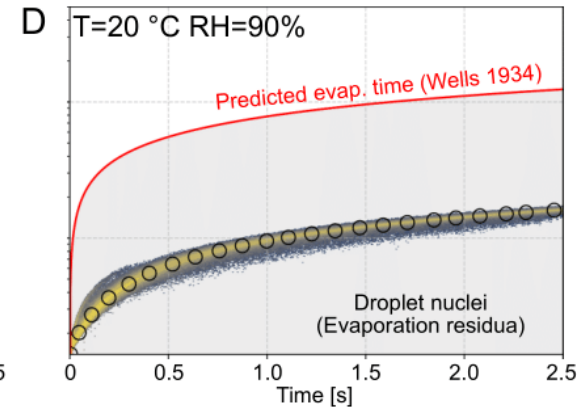
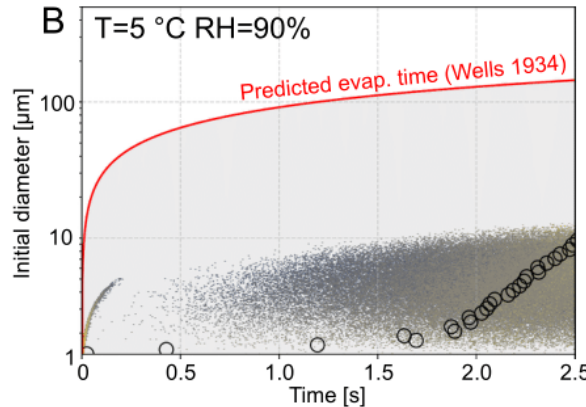
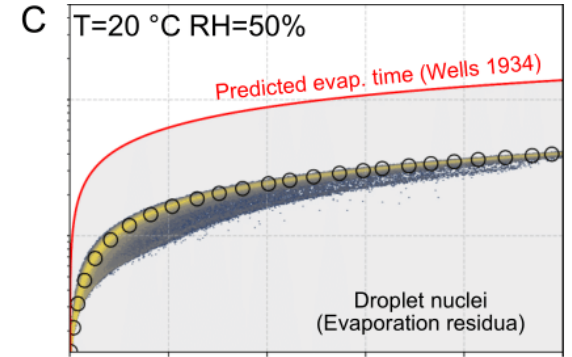
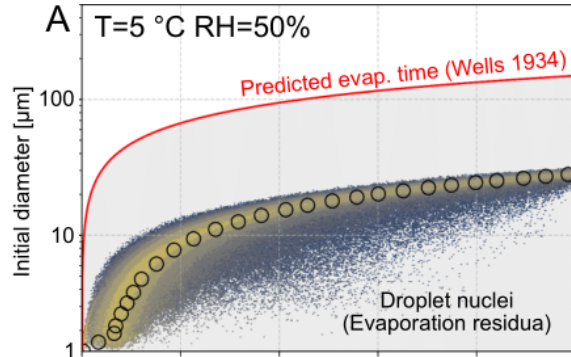
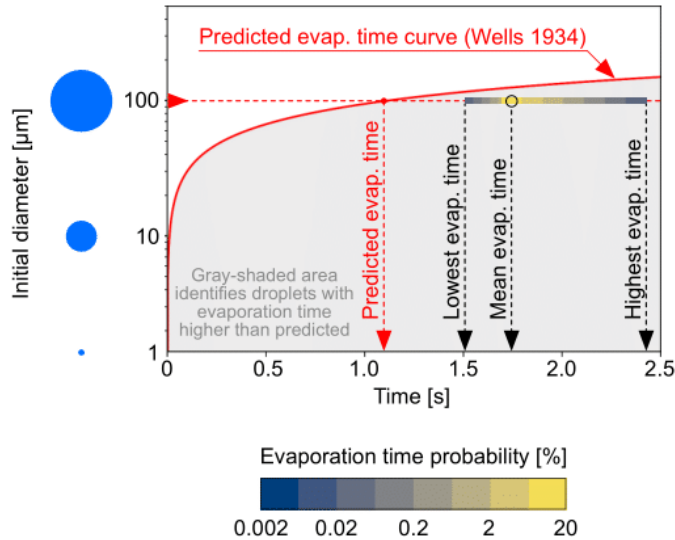
- Two different phases of propagation: jet phase & puff phase. ➡ Project 5
- Both simulations and experiments exhibit a very similar behavior and are in excellent agreement.



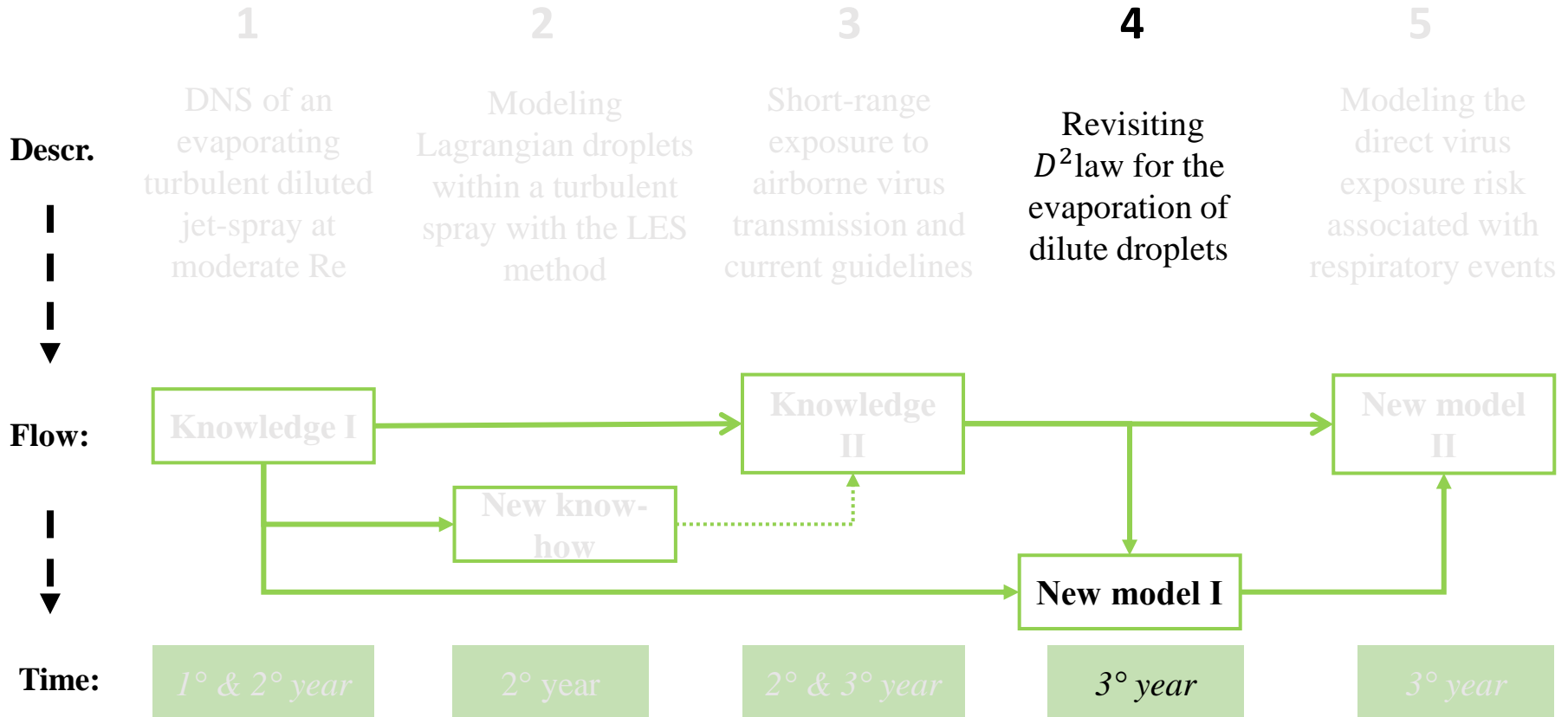
Size threshold  
used in public  
guidelines to  
differentiate  
large droplets  
and aerosols :  
 $5\mu\text{m}$  ?

Time required by the respiratory droplets to complete the evaporation process in the four ambient conditions tested.

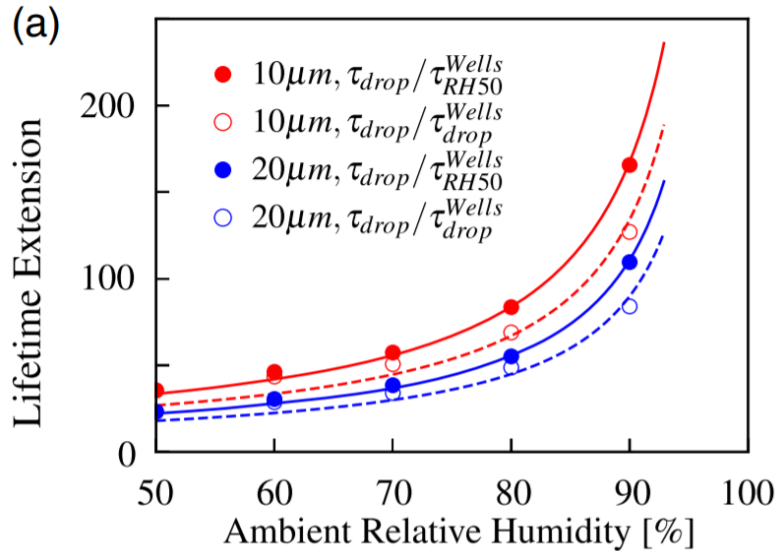
Sample plot (100  $\mu\text{m}$  droplets)



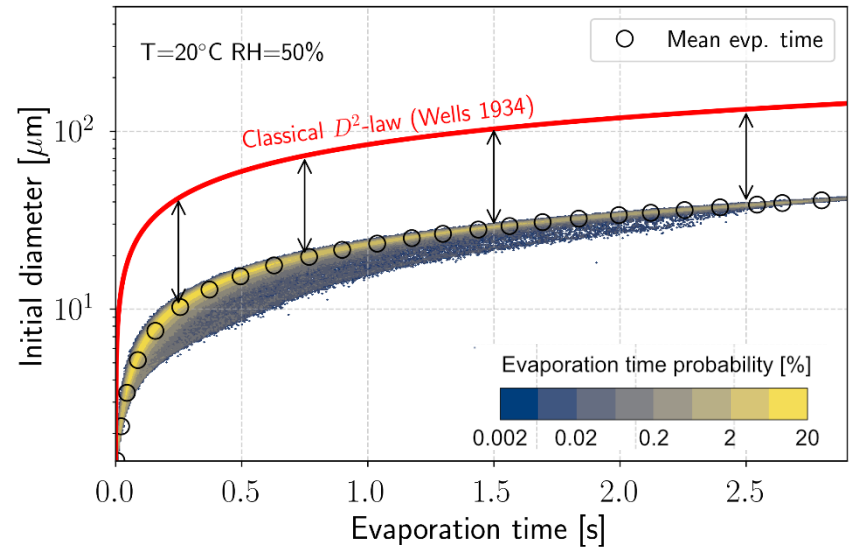
➤ Droplets' lifetime is always about one order of magnitude larger compared to previous predictions by Wells theory, in some cases up to 200 times. (some universality) → Project 4







*Extended lifetime of respiratory droplets as a function of relative humidity up to RH = 90 %*



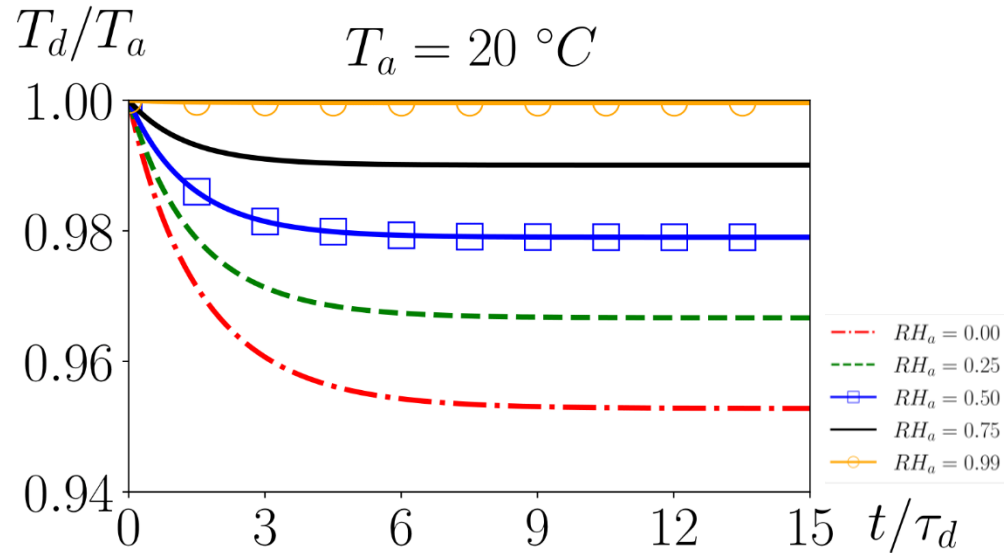
*Evaporation time of respiratory droplets*

- Chong et al. showed that “...droplets have  $O(100)$  longer lifetimes in a turbulent vapor puff at high ambient relative humidity than that predicted by the Well theory...”. Our results confirm this observation.
- Although the resulting evaporation times are much larger than  $D^2$ -law/Wells predictions, it is worth observing that the  $D^2$ -law scaling seems to still bear some universality.

# $D^2$ -law: a revision (very dilute regimes)

## Formulations for droplet evaporation

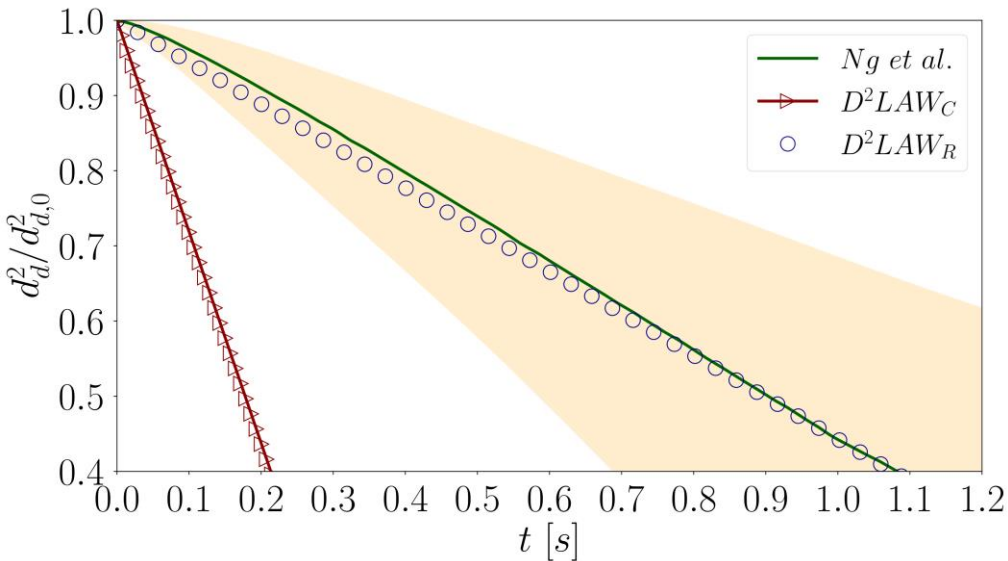
Full coupling	Classical $D^2$ law	Revised $D^2$ law
	$\frac{dr_d^2}{dt} = -K$	
	$K = \frac{Sh \rho_g}{Sc \rho_l} v_g H_m [T_d]$	
$T_d [t]$	$T_d \equiv T_{d,0}$	
	$\equiv T_{g,0}$	$\equiv T_{g,0} - \frac{Sh Pr L_v}{Nu Sc C_{p,g}} H_m$



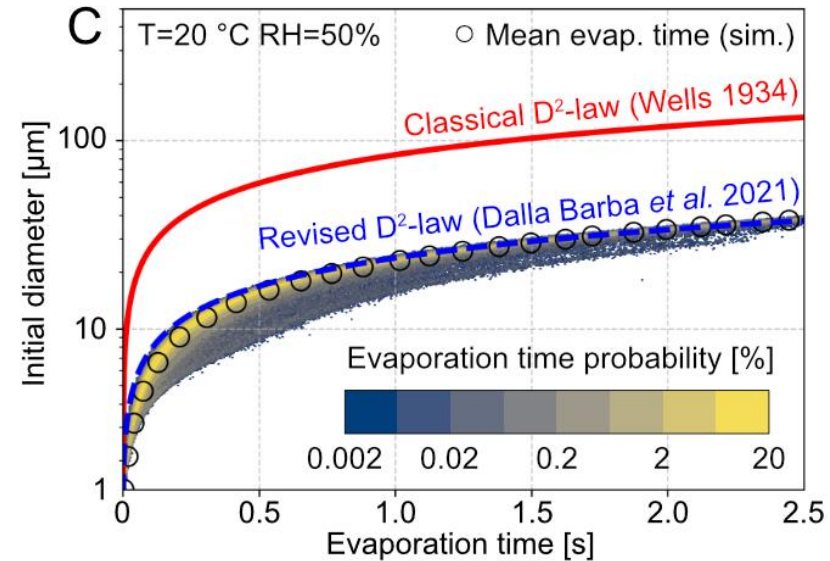
Temporal evolution of the temperature of evaporating water droplets,  $T_d$ , at  $T_a=20^\circ\text{C}$ .

- In our revised  $D^2$ -law the droplet temperature is assumed constant but equal to asymptotic equilibrium **accounting for latent heat**
- $\mathbf{K}$  for  $T_a = 20^\circ\text{C}$  &  $RH_a = 50\%$   $\rightarrow K_c = 4.4 \times 10^{-10}$  ;  $K_r = 1.4 \times 10^{-10}$

## Coughing (*Ng et al.*)

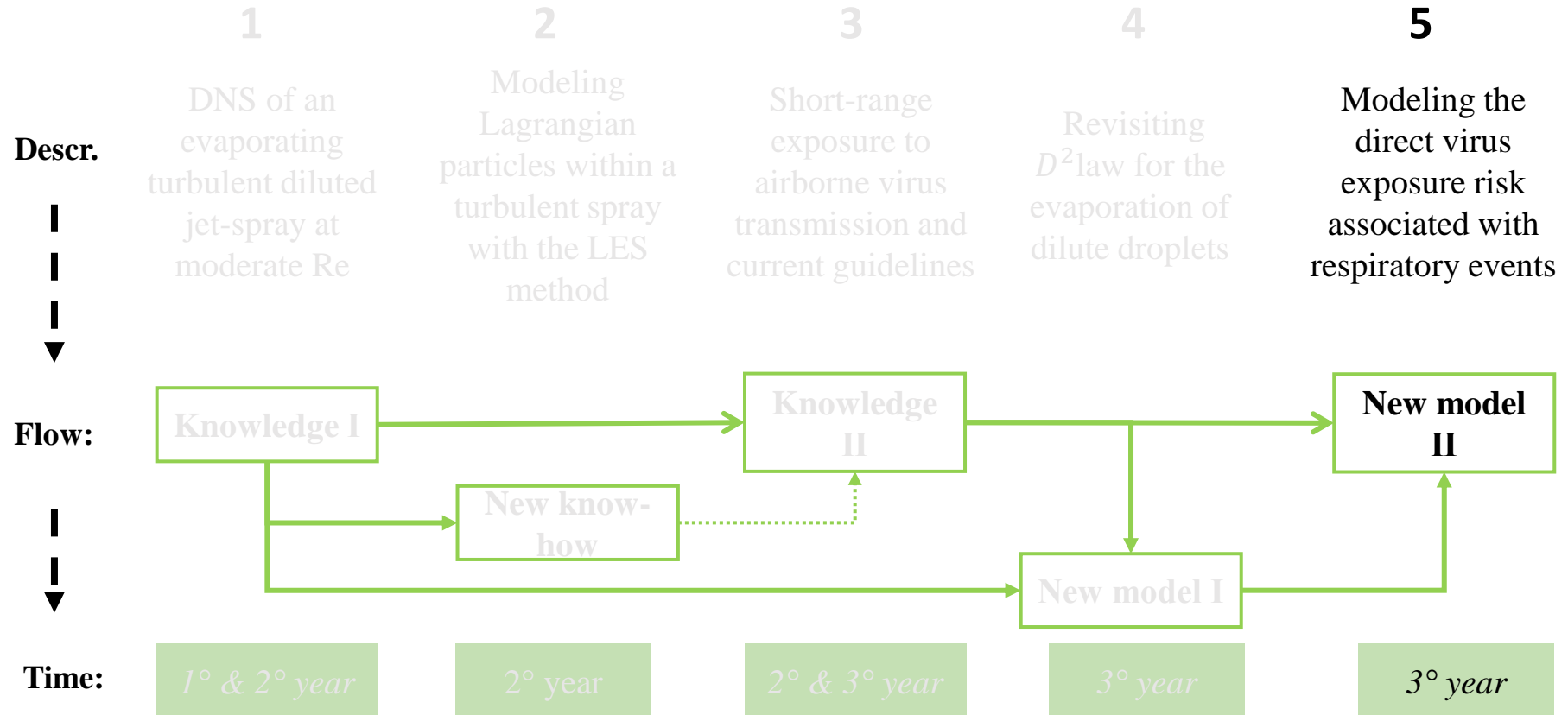


## Sneezing (*Wang et al.*)

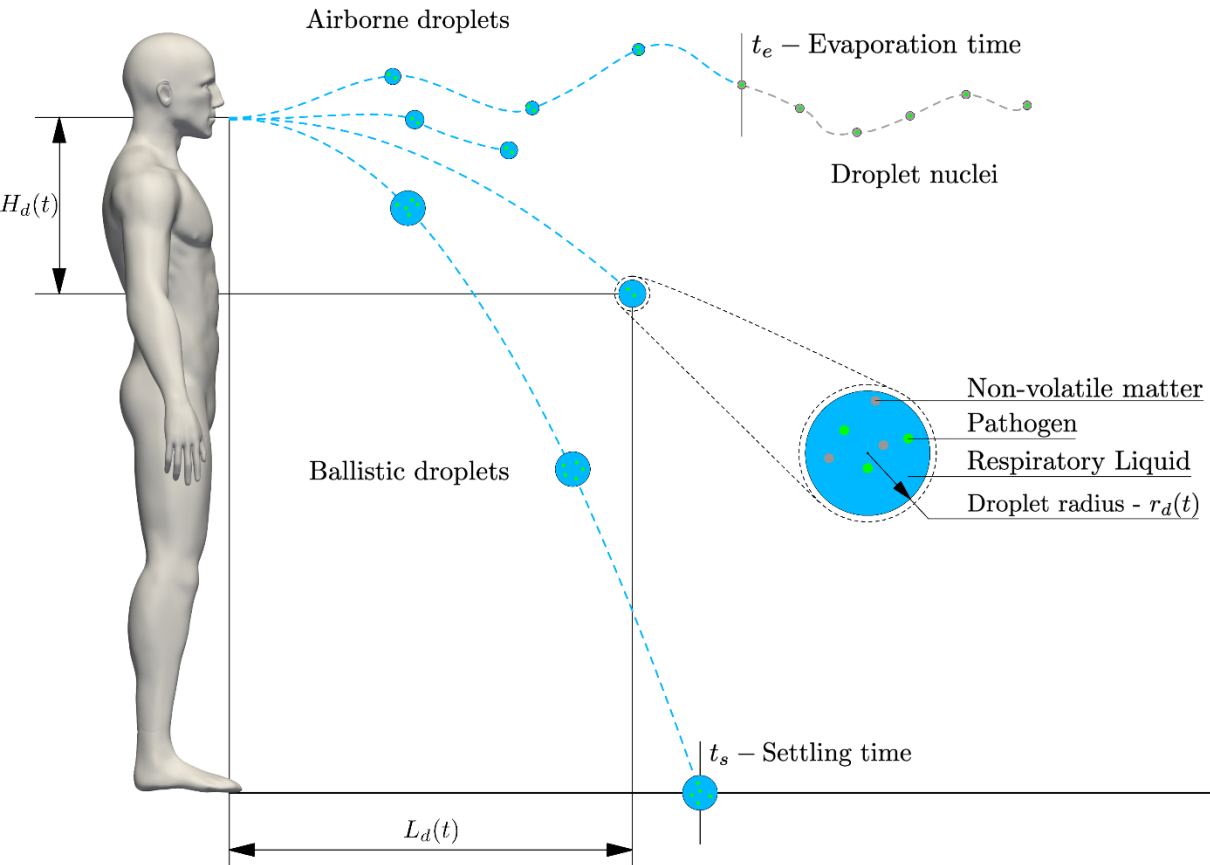


➤ The proposed model is capable to accurately predict the mean evaporation behaviors of respiratory droplets with respect to the traditional  $D^2$ -law /Wells theory.

• *Ng, C. S. et al. (2021). Phys. Rev. Fluids, 6(5), 054303.*



# A new framework for respiratory droplets



➤ Our model includes:

1. a revised  $D^2$ -law;
2. a correction to Stokes law;
3. the two-stage propagation of respiratory events: jet & puff.

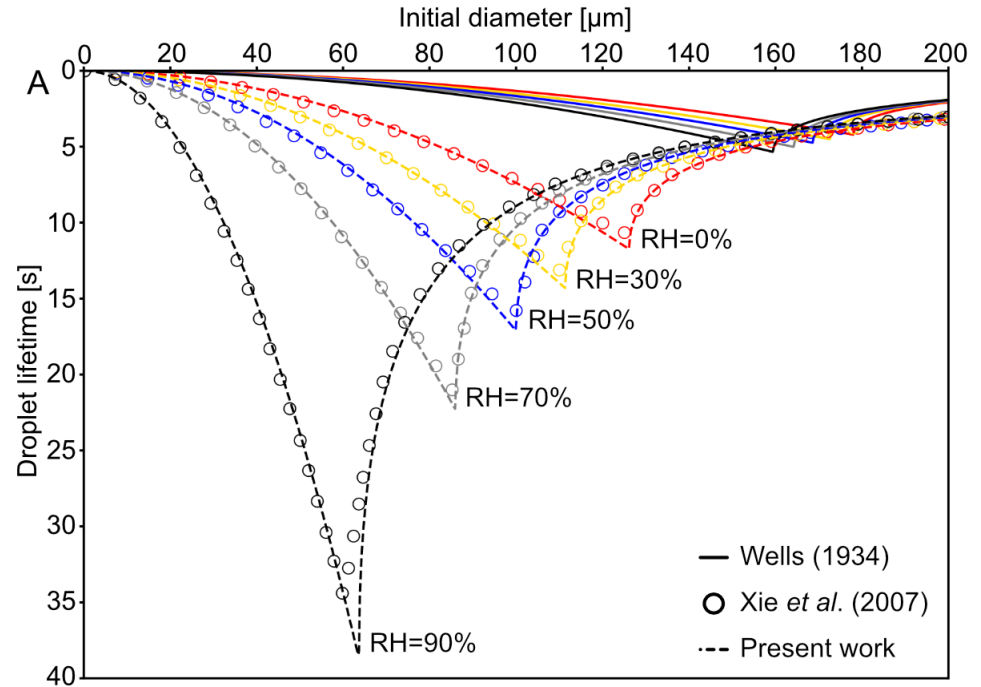
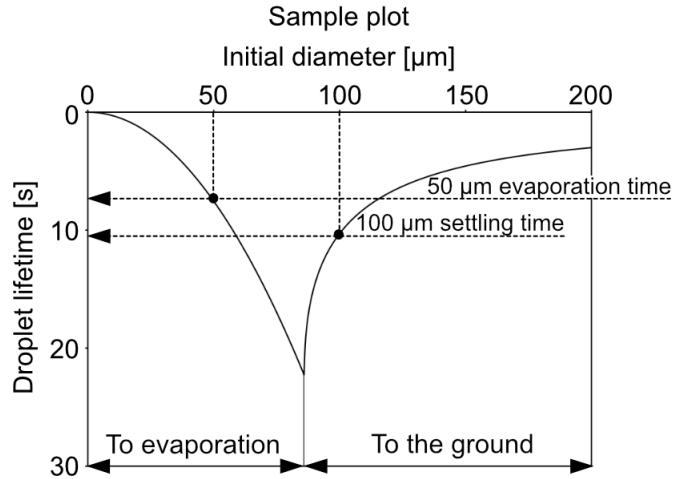
$$t_l = \min(t_e, t_s)$$

$$t_e = \frac{D_{d,0}^2}{k}$$

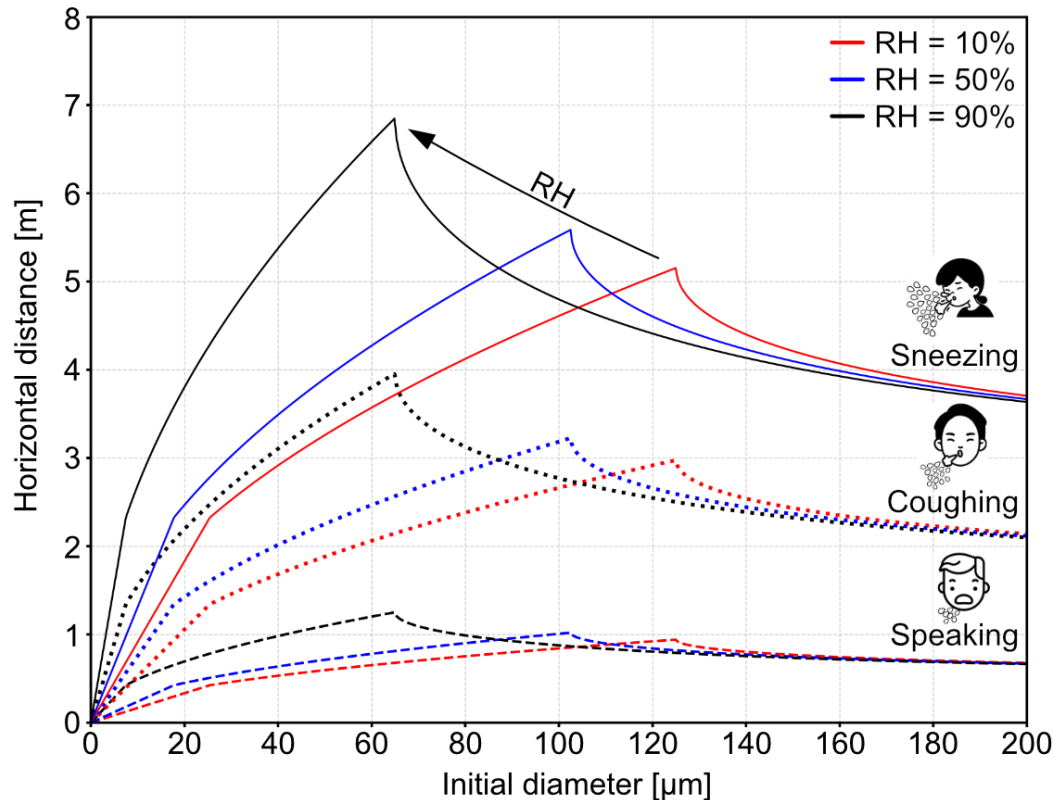
$$t_s = \frac{D_{d,0}^2 - \sqrt{D_{d,0}^4 - 9 \frac{4k \mu}{(\rho_d - \rho) g f} H_d}}{k}$$

$$L_d = \sqrt{4BU_0R_0} t_l^{\frac{1}{2}}, \text{ when } t_l \leq t_{inj}$$

$$\sqrt{4BU_0R_0} t_{inj}^{\frac{1}{4}} t_l^{\frac{1}{4}}, \text{ when } t_l \geq t_{inj}$$



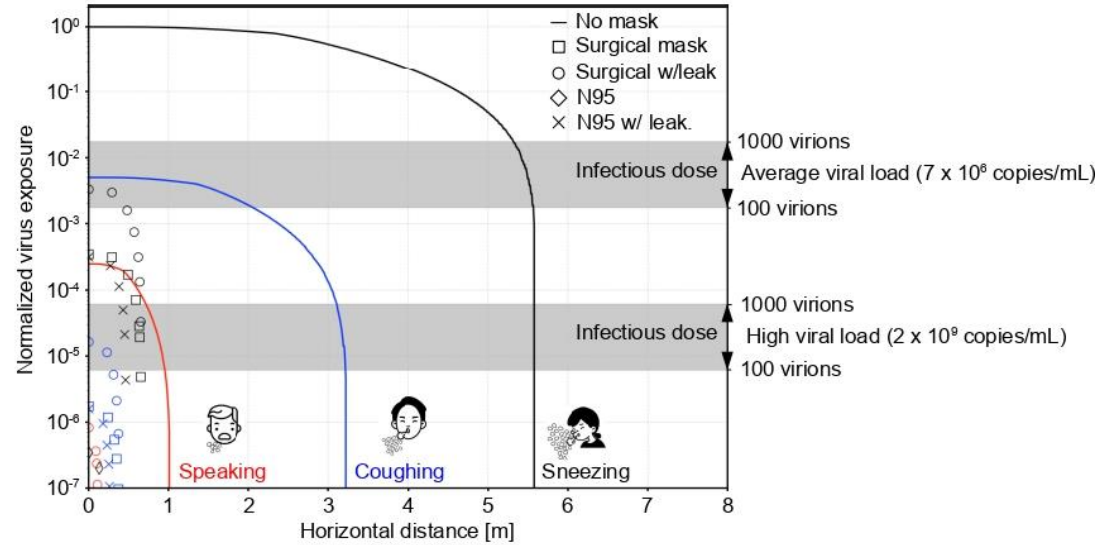
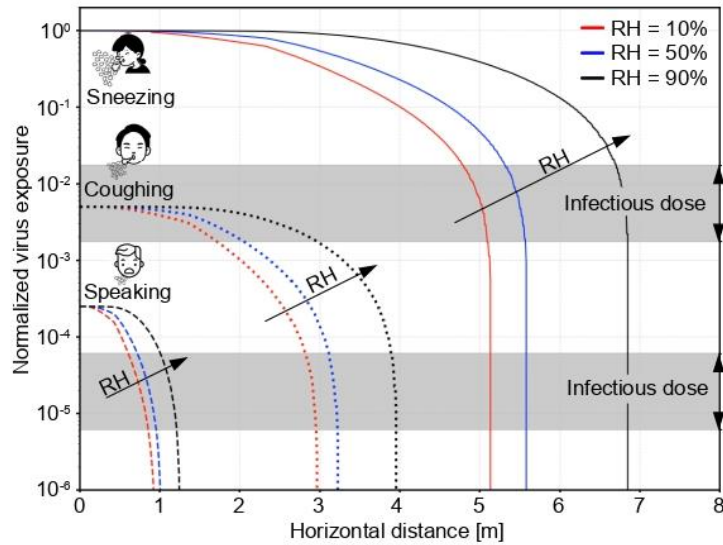
➤ The present results predicted with our model are in excellent agreement with the reference data of Xie *et al.* (2007).



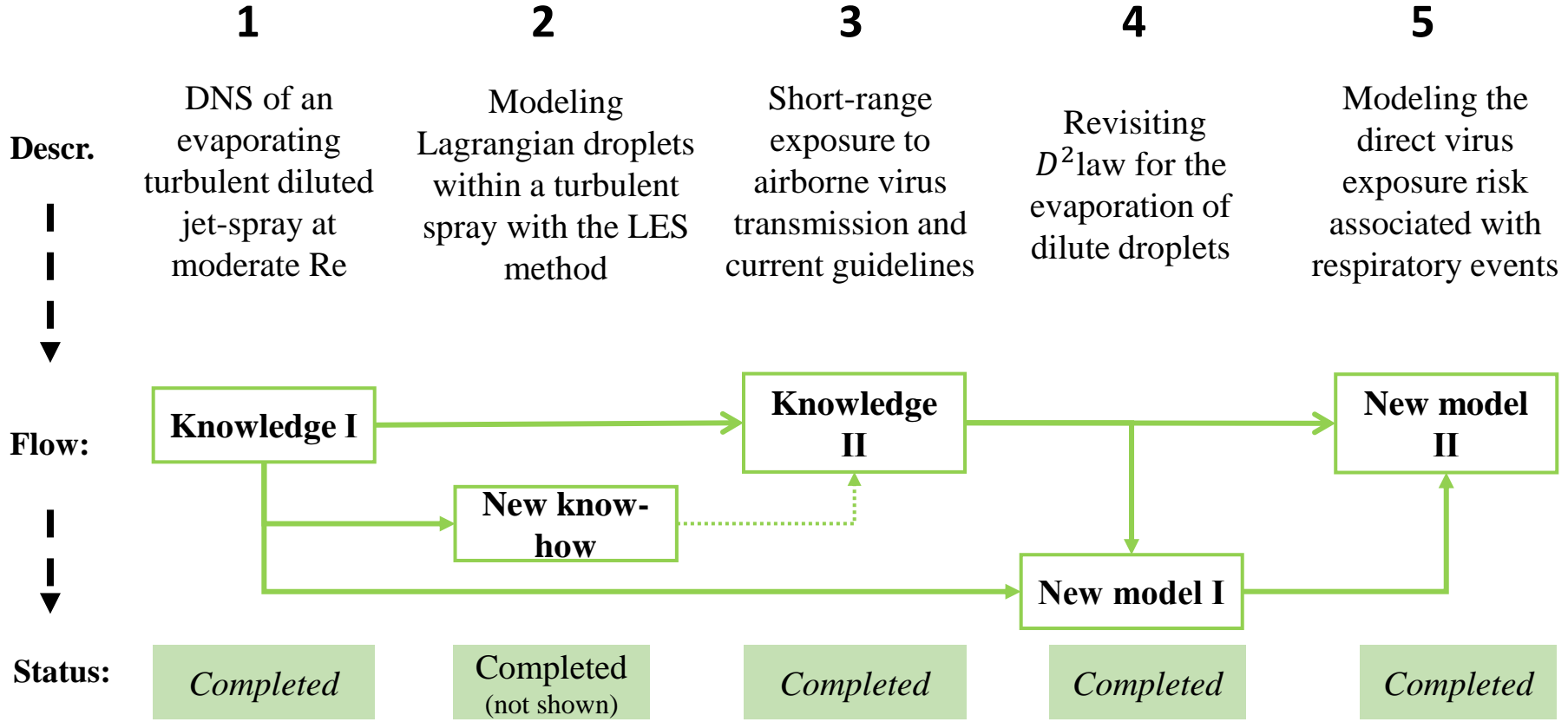
- Max distances:
  - 5-7 m for sneezing
  - 3-4 m for coughing
  - ~1 m speaking
- In Bourouiba's experimental analysis, "...Peak exhalation speeds (*of sneeze*) can reach up to **10-30 m/s**, creating a cloud that can span approximately **7-8 m...**"
- Abkarian, M. et al. reported **1~2 m** distance related to speaking events.
- ✓ The model estimates for speaks and sneezes are consistent with previous experimental findings!



# Physical distancing & face covering



- The exposure risk is impacted by both variables, which indicates the non-existent of a universal safe distance, but more a quantitative reduction of the exposure risk with distance;
- Wearing face marks provides an excellent protection, effectively limiting the infection risk even at short physical distances, i.e. less than 1 meter.





- ✓ We firstly showed that, in a DNS of high-Re turbulent spray, droplets form clusters surrounded by high vapor concentration; the classical evaporation model,  $D^2$ -law, strongly underestimate droplet evaporation time.
- ✓ We performed accurate simulations of droplet-laden turbulent puffs emitted during sneezes in a wide range of environmental conditions.
- ✓ Strong variation in droplets' evaporation or condensation in accordance with their local temperature and humidity microenvironment; and the incorrect definition of aerosols.
- ✓ Models currently used in public health guidelines grossly underestimate, by at least one order of magnitude, the actual evaporation times. Meanwhile the classical theory scaling seems to bear some universality.



- ✓ We revised the classical  $D^2$ -law by a proper estimate of the asymptotic droplet properties, which provides a superior description of droplet evaporation with respect to the classical model;
- ✓ We proposed an effective framework for respiratory droplets to assess the virus infection risk related to the direct contagion route, with which the impact of physical distancing and face-covering on limiting infection risk has been quantified considering different environmental conditions and respiratory events.

## ➤ Publications

- Wang, J. & Picano, F. (2021). Modeling Lagrangian droplets within a turbulent spray with the LES method. In preparation.
- Wang, J., Dalla Barba, F., Roccon, A., Sardina, G., Soldati, A., & Picano F. (2021). Modeling the direct virus exposure risk associated with respiratory events. *J. R. Soc. Interface*, In press.
- Wang, J., Alipour, M., Soligo, G., Roccon, A., De Paoli, M., Picano, F., & Soldati, A. (2021). Short-range exposure to airborne virus transmission and current guidelines. *Proc. Natl. Acad. Sci. U.S.A.*, 118 (37), e2105279118.
- Dalla Barba, F., Wang, J., & Picano, F. (2021). Revisiting D2-law for the evaporation of dilute droplets. *Phys. Fluids*, 33(5), 051701.
- Wang, J., Dalla Barba, F., & Picano, F. (2021). Direct numerical simulation of an evaporating turbulent diluted jet-spray at moderate Reynolds number. *Int. J. Multiph. Flow*, 137, 103567.

## ➤ Conferences (Oral presentation)

- 74th Annual Meeting of the APS Division of Fluid Dynamics, APS, Phoenix, Arizona, November 21-23, 2021.
- 18th Multiphase Flow Conference, HZDR, Online, November 08-12, 2021.
- EUROMECH Colloquium 621: Transport and Flexes in Dispersed Turbulent Flows, EUROMECH, Online, June 30 - July 02, 2021
- 1st BICTAM-CISM Symposium on Dispersed Multiphase Flows: From Measuring to Modeling, BICTAM-CISM, Online, March 02-05, 2021.



- The project is ongoing mainly thanks to:
  - the group at University of Padova: Prof. Francesco Picano and Dr. Federico Dalla Barba;
  - the group in TU Vienna: Prof. Alfredo Soldati and his group members;
  - Other involved colleagues: Prof. G. Sardina, Dr. G. Soligo, Dr. M. Alipour, Dr. M. De Paoli;
  - Financial funding from CSC: #201806250023;
  - Computer resources by PRACE COVID-19 grant: COVID-DROPLETS; by the ISCRA-C project in CINECA: HiReS (HP10C3YNLC) & SnzEnv (HP10C1XSJU)





# Thanks for the attention

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