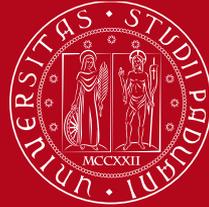


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# High-fidelity simulation and modeling of turbulent sprays

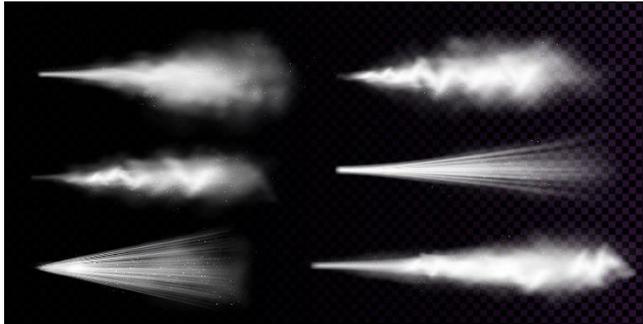
Xiang'en Kong - 38th Cycle

Supervisor: Prof. Francesco Picano

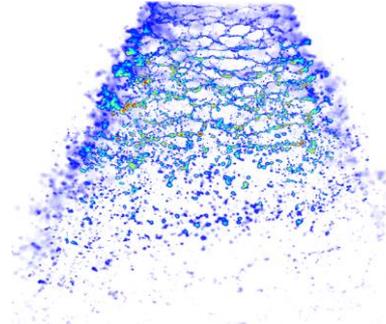
Co-supervisor: Prof. Federico Dalla Barba

Meeting - 16/09/2024

## Spray:



[https://www.freepik.com/free-vector/white-dust-spray-isolated-transparent-background-realistic-set-smoke-powder-with-particles-splash-from-aerosol-stream-spraying-cosmetic-fragrance-deodorant\\_10308169.htm](https://www.freepik.com/free-vector/white-dust-spray-isolated-transparent-background-realistic-set-smoke-powder-with-particles-splash-from-aerosol-stream-spraying-cosmetic-fragrance-deodorant_10308169.htm)

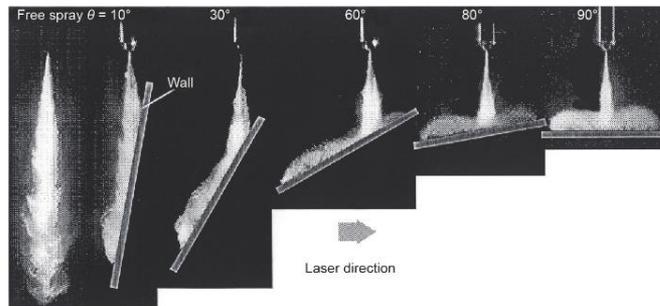


<https://spray-imaging.com/>



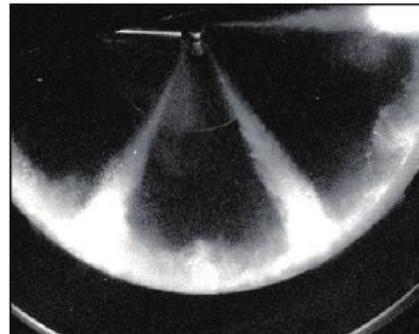
<https://gfycat.com/impartialminoramericanbobtail-flamelet-generated-manifolds-large-eddy-simulation>

## Particles in Wall-Bounded Turbulent Flows:



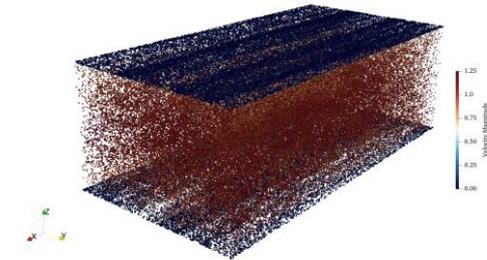
doi: [10.1016/j.eng.2019.04.010](https://doi.org/10.1016/j.eng.2019.04.010)

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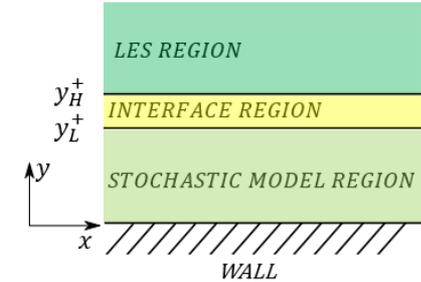
doi: [10.1016/j.eng.2019.04.010](https://doi.org/10.1016/j.eng.2019.04.010)

High-fidelity simulation and modeling of turbulent sprays



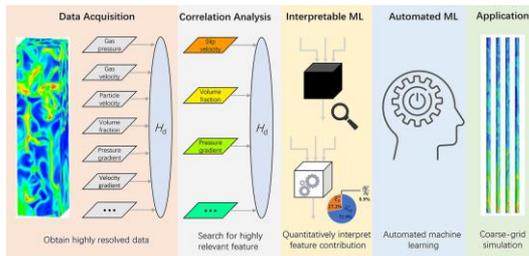
## Task 1:

Modeling dispersed phase transport in Wall-Model Large-Eddy-Simulations



## Task 2:

Near-wall transport of dispersed multiphase flows simulation using Machine-learning algorithms



## Task 3:

Simulation of dispersed multiphase flows (spray, particle-laden channel) using physics-based and machine-learning algorithms

[j.partic.2022.12.004](http://j.partic.2022.12.004)

## □ DNS:

Accurate simulation, but very computationally expensive

## □ RANS:

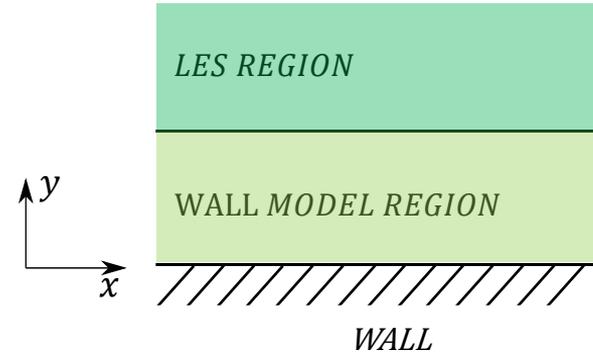
Low computational cost but lack of fidelity

## □ LES:

Better accuracy than RANS but high computational cost for high Reynolds numbers wall bounded flows

## □ Wall-Model Large-Eddy-Simulations (WM-LES)

Better accuracy than RANS with lower computational cost at wall than LES



## WM-LES

- ❑  $N_x \times N_y \times N_z = 48 \times 48 \times 48$  **LOW RES!!!**
- ❑  $L_x \times L_y \times L_z = 6h \times 2h \times 3h$
- ❑  $Re_\tau = 1000$
- ❑  $N_p = 300000$
- ❑  $St^+ = 1, 10, 100$
- ❑ **Wall-modelled layer  $y^+ < 100$  both for carrier and discrete phase (below 2.5 nodes)**

$$Re_\tau = \frac{u_\tau h}{\nu} \quad St^+ = \frac{\tau_p}{\tau^+}$$

## PRELIMINARY REFERENCE DNS

- ❑  $N_x \times N_y \times N_z = 1216 \times 512 \times 640$
- ❑  $L_x \times L_y \times L_z = 10h \times 2h \times 3h$
- ❑  $\Delta y_{min}^+ \simeq 0.5$
- ❑  $Re_\tau = 1000$
- ❑  $N_p = 300000$
- ❑  $St^+ = 1, 10, 100$

## □ Navier-Stokes (incompressible) (WM-LES)

$$\nabla \cdot \tilde{\mathbf{u}} = 0$$

$$\rho \frac{\partial \tilde{\mathbf{u}}}{\partial t} = -\nabla p + \nabla \cdot [2(\mu + \mu_{SGS})\tilde{\mathbf{E}}]$$

$\mu_{SGS}$ : Sub-grid viscosity with **WALE**

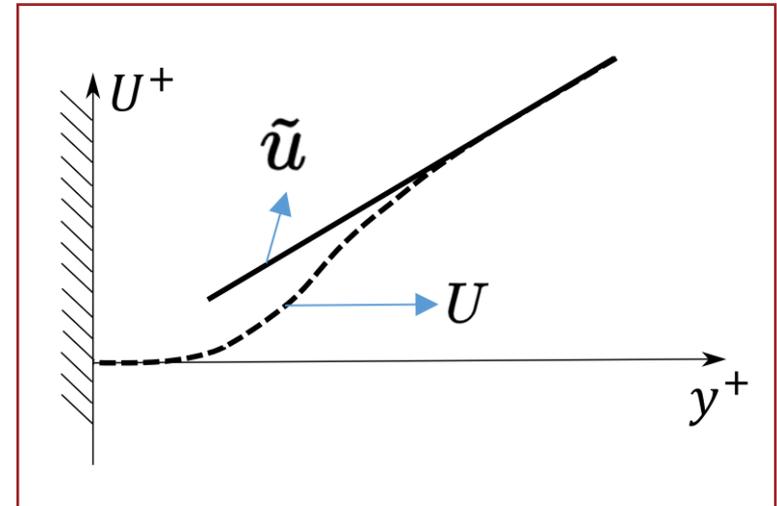
$\tilde{\mathbf{E}}$ : Deformation tensor

## □ Lagrangian Point-particle equations

$$\frac{dv}{dt} = f_p \frac{u - v}{\tau_p} \quad u = \tilde{u} + u''$$

If  $u'' = 0$ , SGS fluctuation is neglected

## □ Algebraic Wall-model



## Lagrangian Point-particle equations

$$\frac{dv}{dt} = f_p \frac{u - v}{\tau_p}$$

$$u = U + u_{STO}$$

$$f_p = 1 + 0.15 Re_p^{0.687}$$

$$Re_p = \frac{2||u - v||r_p}{\nu}$$

- $u$  fluid velocity at particle
- $v$  point-particle velocity
- $U$  averaged fluid velocity fields
- $u_{STO}$  stochastic velocity fluctuations at the particle positions
- $\tau_p$  particle relaxation time
- SGS fluctuations are neglected

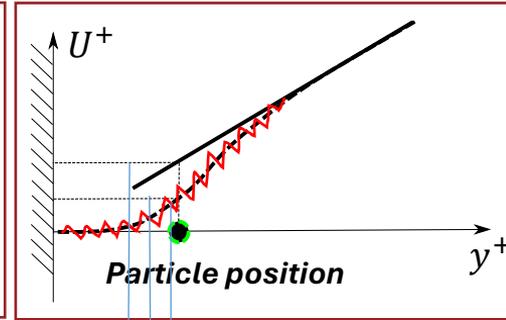
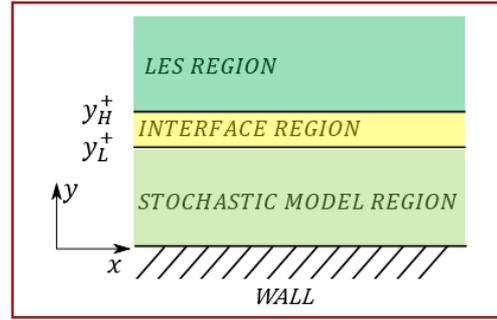
## The normalized Langevin equations

$$d\left(\frac{u_{STO}}{\sigma_x}\right) = -\left(\frac{u_{STO}}{\sigma_x}\right) \frac{dt}{\tau_l} + \sqrt{\frac{2}{\tau_l}} d\xi_x + \frac{\partial\left(\frac{\overline{uv}}{\sigma_x}\right)}{\partial y} \frac{dt}{1+St}$$

$$d\left(\frac{v_{STO}}{\sigma_y}\right) = -\left(\frac{v_{STO}}{\sigma_y}\right) \frac{dt}{\tau_l} + \sqrt{\frac{2}{\tau_l}} d\xi_y + \frac{\partial\sigma_y}{\partial y} \frac{dt}{1+St}$$

$$d\left(\frac{w_{STO}}{\sigma_z}\right) = -\left(\frac{w_{STO}}{\sigma_z}\right) \frac{dt}{\tau_l} + \sqrt{\frac{2}{\tau_l}} d\xi_z$$

$\sigma_x, \sigma_y, \sigma_z$  RMS of velocity fluctuations

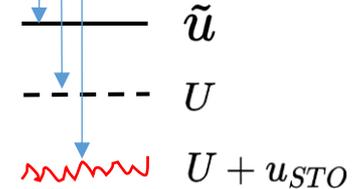


Drift correction terms

$$St = \tau_p / \tau_l$$

Lagrangian time scale

Gaussian random numbers with zero mean and variance dt

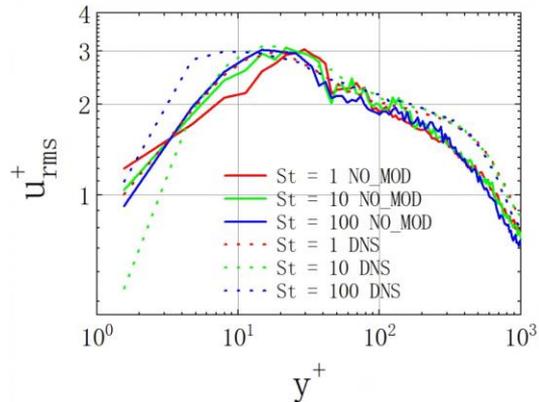
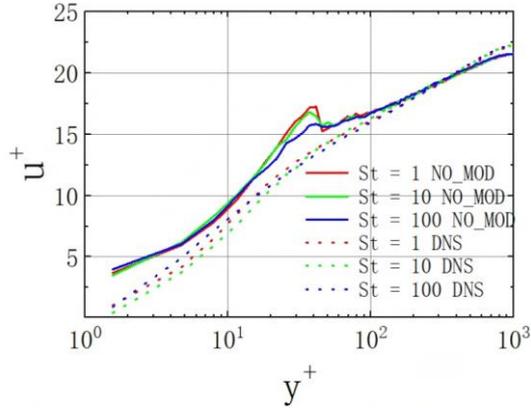


$$u_{CMB} = \sqrt{\alpha} u_{LES} + (1 - \sqrt{\alpha}) u_{AVG} + \sqrt{1 - \alpha} u_{STO}$$

Dehbi, A. (2010). Validation against DNS statistics of the normalized Langevin model for particle transport in turbulent channel flows. Powder Technology, 200(1-2), 60-68.

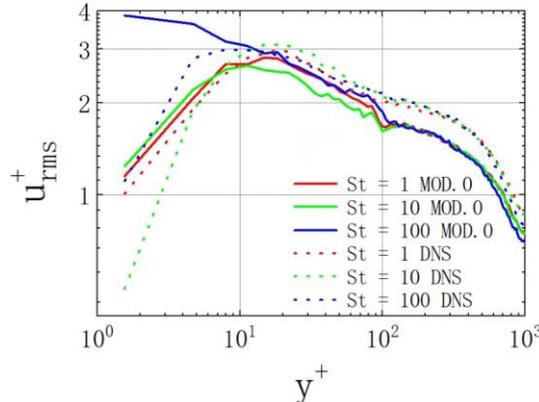
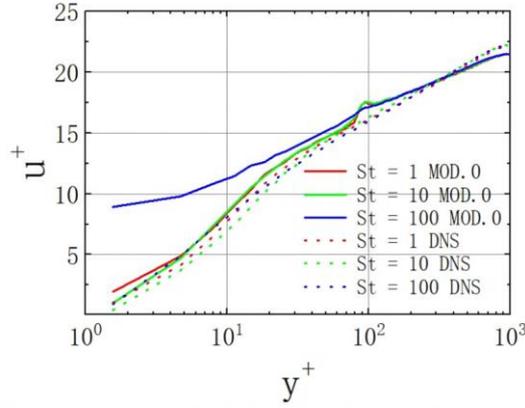
# Task 1: Velocity Statistics

## NO MODEL



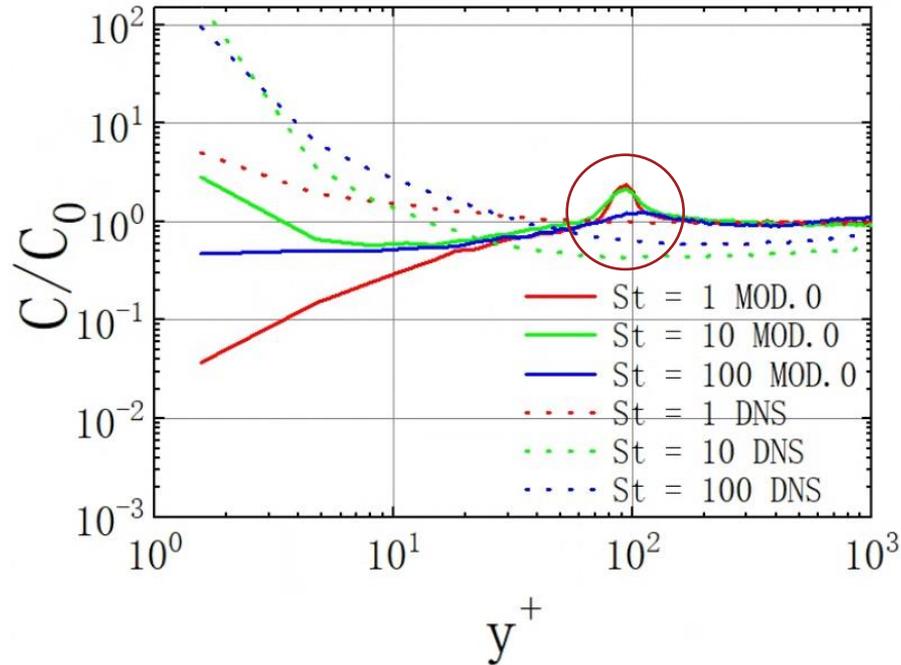
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## STOCHASTIC MODEL

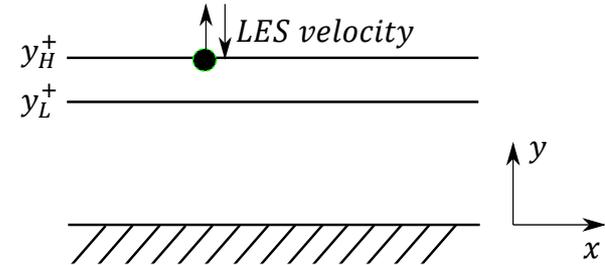


High-fidelity simulation and modeling of turbulent sprays

□ For all Stokes numbers, there are apparent difference in velocity and  $u_{RMS}$  !



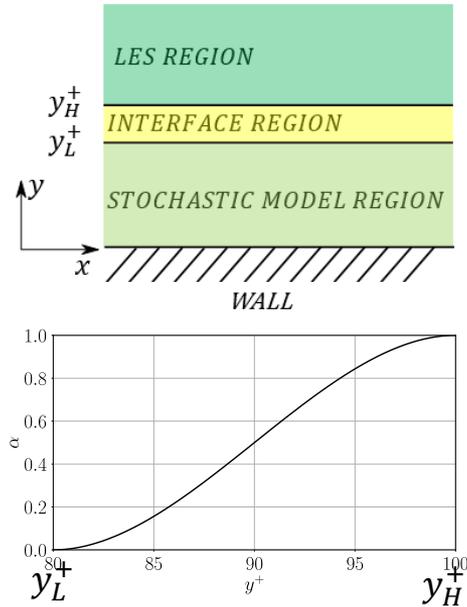
Particle velocity



Particles going outside of interface may encounter fluid velocity fluctuations with opposite sign (phase opposition) thus stopping the particles at the interface for longer time!

**In the interfacial region, the normalized concentrations of all Stokes peaked and deviated from DNS results!**

# Task 1: WM-LES—A Semi-stochastic Approach 1/2



$$\alpha = \begin{cases} 1, & y^+ \geq y_H^+ \\ 3t^2 - 2t^3, & y_L^+ \leq y^+ < y_H^+ \\ 0, & y^+ < y_L^+ \end{cases}$$

$$t = 1 + \frac{(y^+ - y_L^+ - (y_H^+ - y_L^+))}{y_H^+ - y_L^+}$$

For streamwise and spanwise velocity

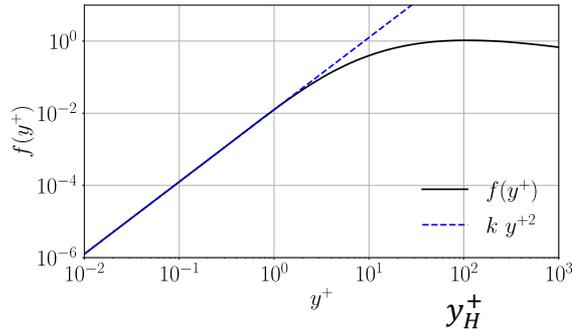
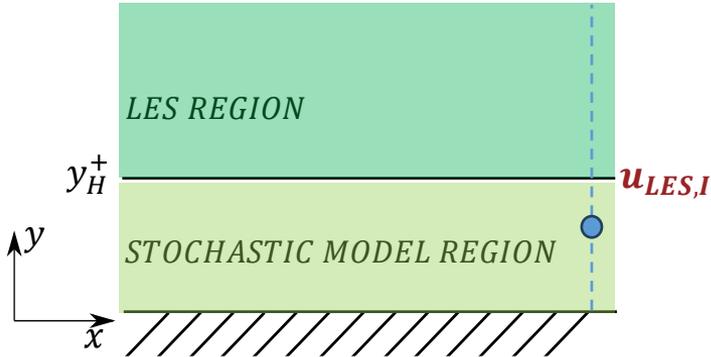
$$\frac{dv}{dt} = f_p \frac{u - v}{\tau_p} \quad \left| \quad u = \begin{cases} \tilde{u} + u'', & y_p^+ \geq y_H^+ \\ u_{CMB}, & y_L^+ \leq y_p^+ < y_H^+ \\ U + u_{STO}, & y_p^+ < y_L^+ \end{cases}$$

$$f_p = 1 + 0.15 Re_p^{0.687}$$

$$Re_p = \frac{2||u - v||r_p}{\nu}$$

$$u_{CMB} = \sqrt{\alpha} \tilde{u} + (1 - \sqrt{\alpha}) U + \sqrt{1 - \alpha} u_{STO}$$

The difference between previous and present model lies in the method of calculating normal velocity.



**For normal velocity:** Modulated from the interface LES value

$$\frac{dv}{dt} = f_p \frac{u - v}{\tau_p}$$

$$f_p = 1 + 0.15 Re_p^{0.687}$$

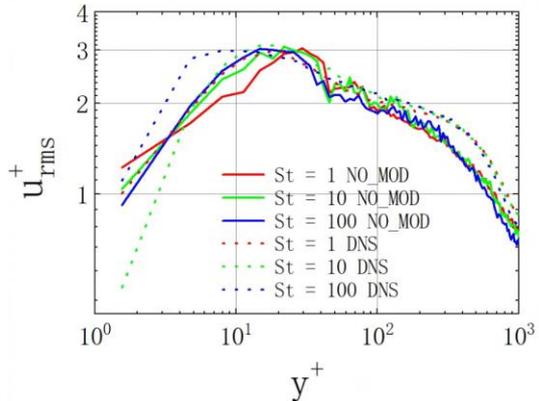
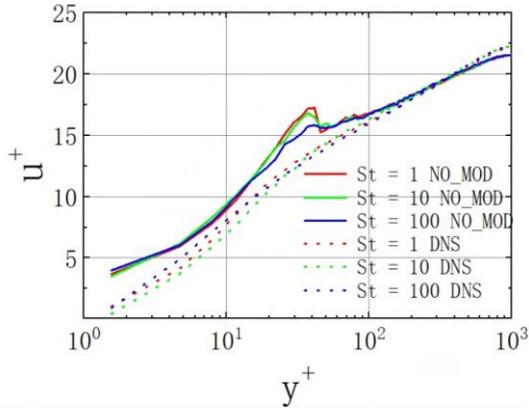
$$Re_p = \frac{2||u - v||r_p}{\nu}$$

$$u = \begin{cases} \tilde{u} + u'', & y_p^+ \geq y_H^+ \\ u_{FUN}, & y_p^+ < y_H^+ \end{cases}$$

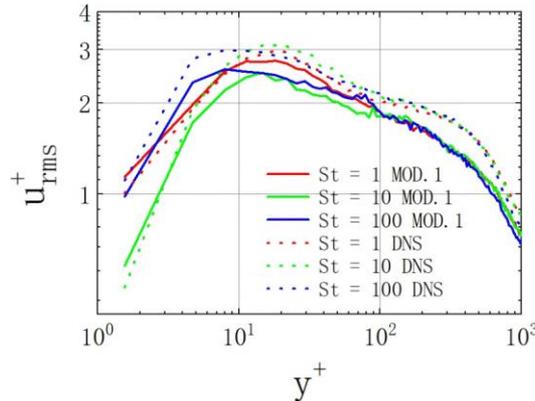
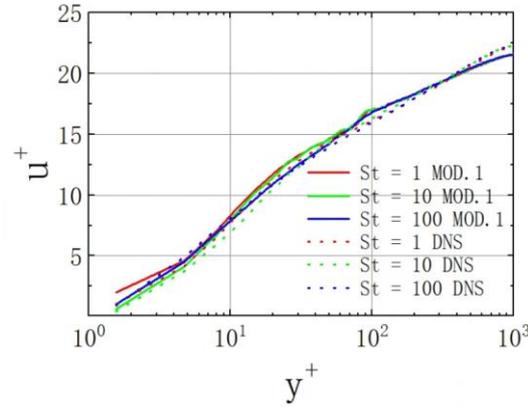
$$u_{FUN} = f(y_p^+) u_{LES,I} + k f(y_p^+) \left. \frac{df(y^+)}{dy^+} \right|_{y_p^+} \frac{\Delta t}{1 + St^+} + N$$

- $u_{LES,I}$  interpolated from LES velocity field at the interface at  $y_H^+$  (above particle)
- Function  $f(y^+)$  such that:
  - $f(y_H^+) = 1$
  - Quadratic trend near zero
  - Derivative modulated by Stokes  $St^+ = \tau_p/\tau^+$

## NO MODEL

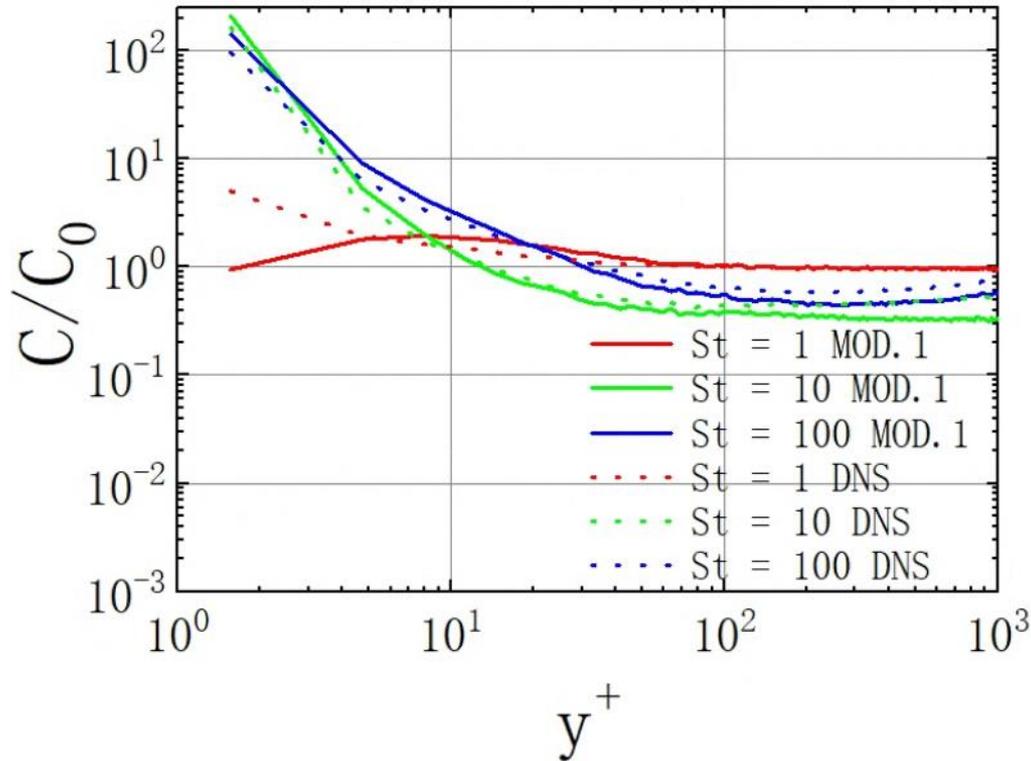


## SEMI-STOCHASTIC



□ Much better agreement!

□ OBS: Lower velocity statistics due to low resolution in LES!



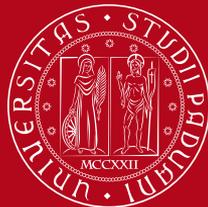
□ Much better agreement of normalized concentrations!

- I. We developed a model for the near-wall numerical treatment of point-particle/droplet-laden flows in Wall-Modelled Large Eddy Simulation (WM-LES). Models **blending a stochastic approach**, i.e. the Langevin equations, **with properly rescaled LES velocity fields along the wall-normal direction**
- II. A machine learning model will be developed for the high-fidelity simulation of **particle-laden flow near the wall**
- III. A machine learning model will be developed for the high-fidelity simulation of **turbulent sprays**



# Thanks for the attention

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