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# Advanced technologies for carbon capture and biohydrogen production

Alessandro Crescenzi - 40th Cycle

Supervisor: Prof. Francesco Picano

Co-supervisor: Prof. Federico Dalla Barba - Dott. Graziano Tassinato

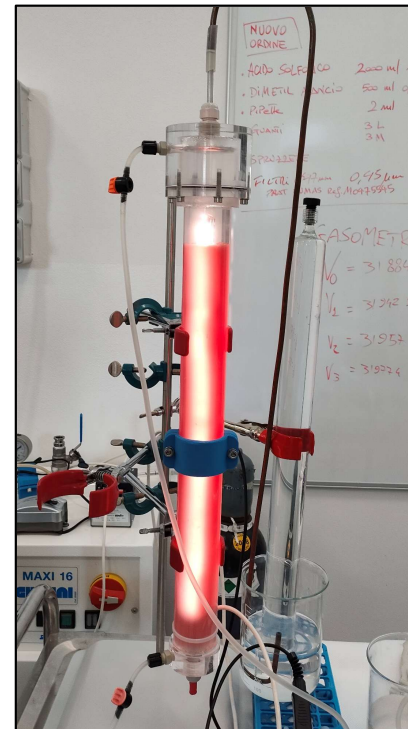
Admission to the 2<sup>nd</sup> year - 14/10/2025



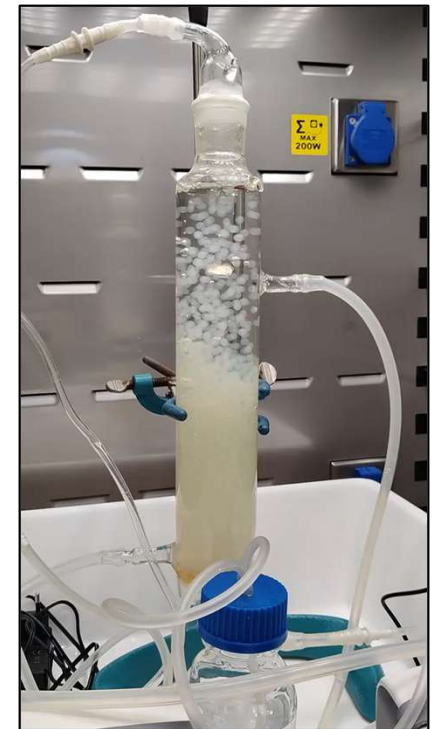
## Doctoral work motivation and objective



- Develop **CFD models** of **column-type bioreactors**.
- The research involves both reactors with a **fixed solid phase** (porous matrix) and ones with a **dispersed solid phase**.
- The **red bacteria (PNSB)** reactor produces hydrogen and has a solid matrix immersed in culture medium.
- The **microalgae** reactor gives oxygen and contains small spheres, free to move with the motion of water and bubbles.
- Both feature a **multiphase flow** comprising **gas, liquid and solid phases**.



PNSB reactor

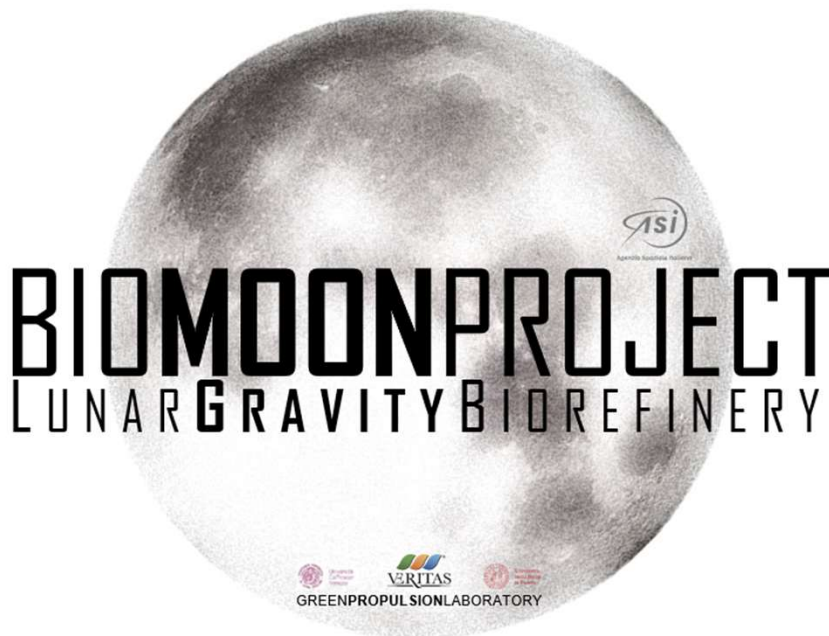


Microalgae reactor



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## Industry collaborations



- Project developed by **Veritas S.p.A.**, commissioned by **Agenzia Spaziale Italiana (ASI)**.
- Aim to develop a **biorefinery** that uses **microorganisms** to process **waste** produced by astronauts and produce **nutrients and resources**.
- Collaboration with:
  - **Green Propulsion Laboratory** (Veritas S.p.A., Fusina) → Construction of a prototype space model;
  - **Università Ca' Foscari** → Experimentation on microorganisms in a laboratory-scale system;
  - **UniPD** → Fluid dynamics and energy modelling of the system.



## Task #1: Macroscopic model development

- State of the art
- Multiphase flow study
  - Two Dimensional
  - Three Dimensional
- Ansys Fluent model development
- Model validation
- Improvement study
- Reduced gravity study

## Task #2: BIOMOON experiments

- Tests with previous experiments
- Research and selection of suitable equipment
- Validation of the experimental set
- Data collection
- Improvement tests

## Task #3: Microscopic model development

- State of the art
- Model development with in-house software (CaNS)
- Reduced gravity study



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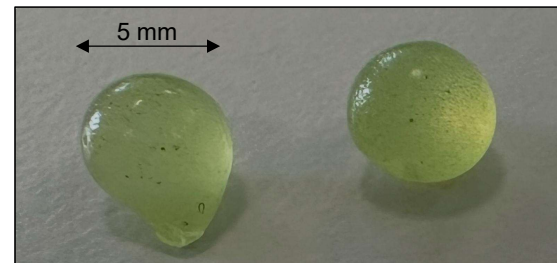


# Task #1



- Modelling a **multiphase bioreactor** is complex, especially with “big particles”
- **Ansys Fluent** commercial software allows to represent the behaviour of the various phases, including **bubble motion, transport in porous media and mass transport phenomena**.
- For gas-liquid-solid systems, **different multiphase models can be used**, each with advantages and limitations:

Model	Description	Pros	Cons
<b>Volume of Fluid (VOF)</b>	Finely resolved interface (useful for few and large bubbles)	High precision and accuracy of the interface	Expensive and not scalable for numerous bubbles
<b>Eulero-Lagrange (DPM)</b>	Continuous liquid phase, bubbles traced as discrete particles	Details on trajectories and forces on particles	More computationally expensive in certain case studies
<b>Eulero-Eulero</b>	Each phase treated as continuously interpenetrating	Robust, suitable for large volumes	Minor detail on the dynamics of individual bubbles



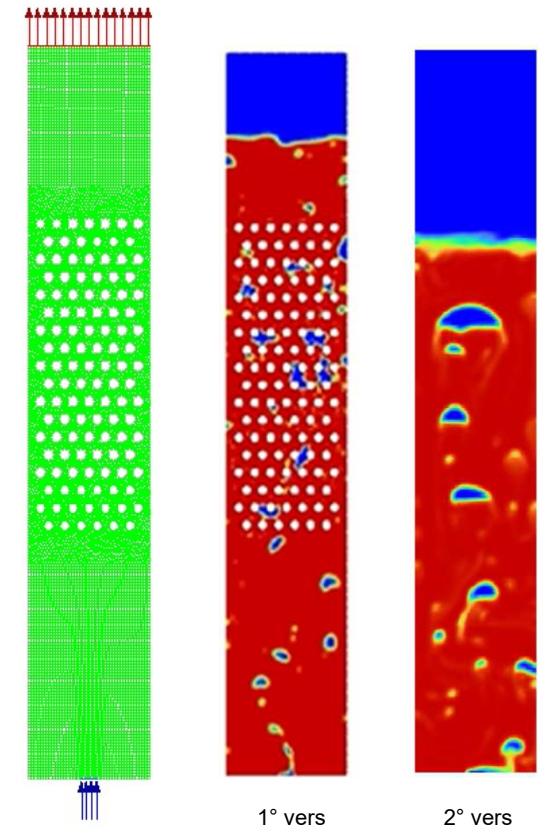


## VOF approach

- 2 versions:
  - Dispersed phase
  - Porous media
- **Abandoned** when GpLab told us **priority** was on the **microalgae reactor**, in combo with VOF being very heavy for our cases

## Eulerian approach

- Single **bubble/sphere tracing is lost**. Phases are still distinct and have their own equations for the conservation of mass, momentum and energy.
- Interactions between phases, such as friction, heat exchange and mass transfer, are modelled using specific exchange terms. This model allows for **detailed analysis of fluidisation and sedimentation**.



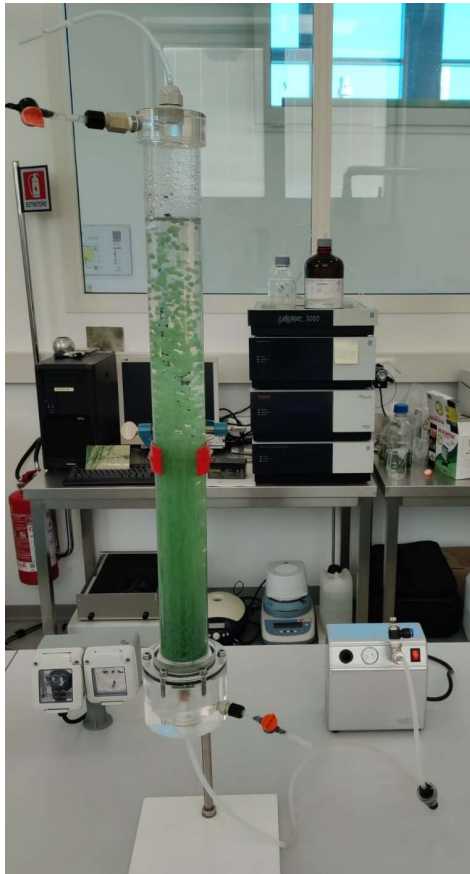


## Eulerian approach

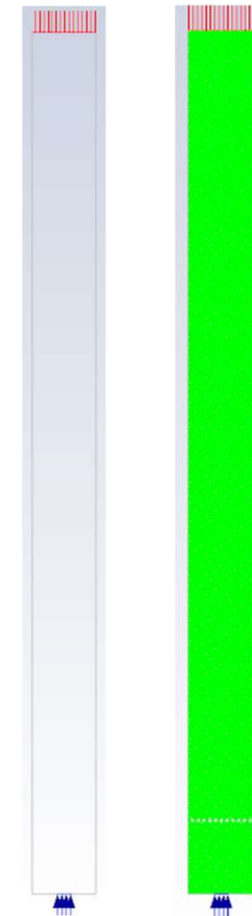
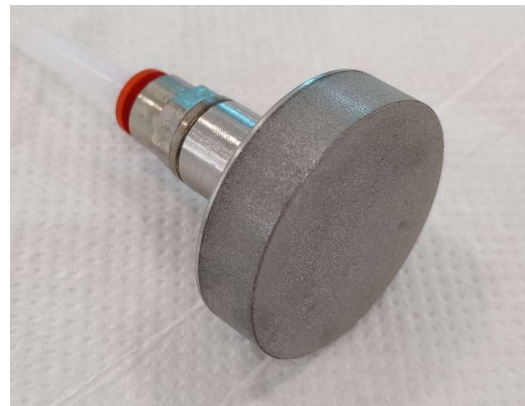
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- Interactions between phases, such as friction, heat exchange and mass transfer, are modelled using specific exchange terms. This model allows for **detailed analysis of fluidisation and sedimentation**.
- **Test sequence** to correctly implement the three-phase problem:
  - Inlets
  - Turbulence models
  - Solid phase dimensions
  - Different gravities
  - Particle mass density
  - Mesh quality



## Current results (2D)



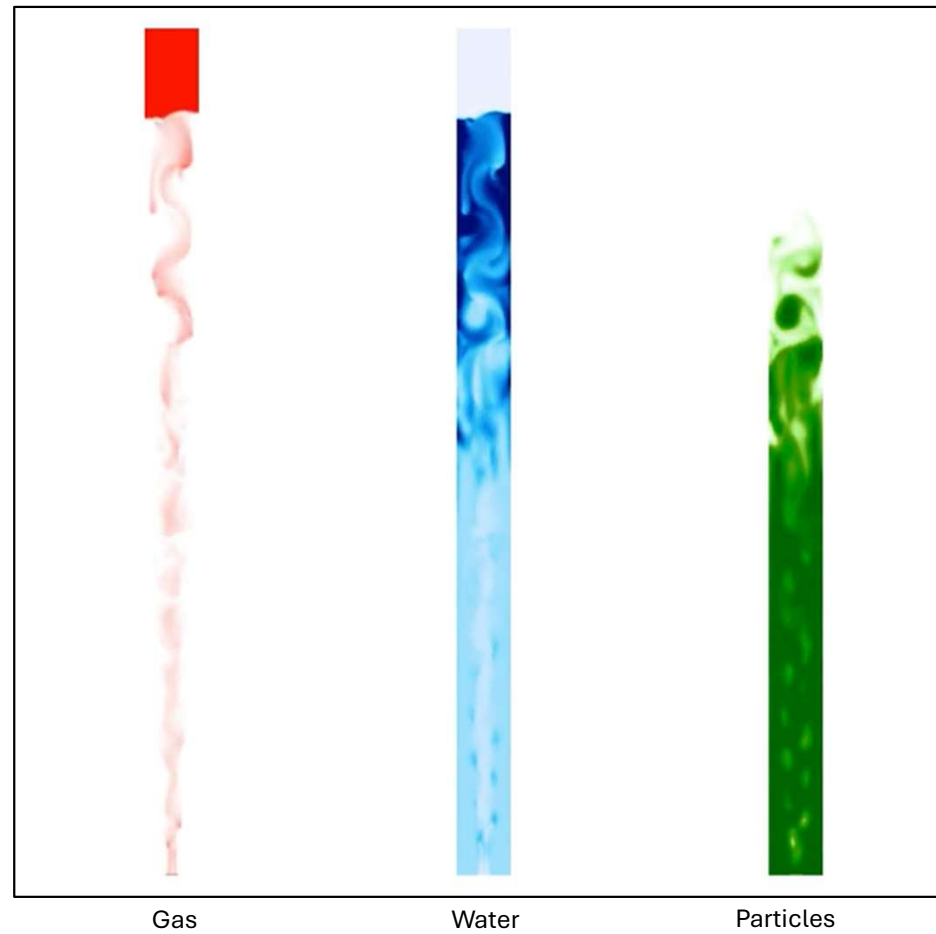
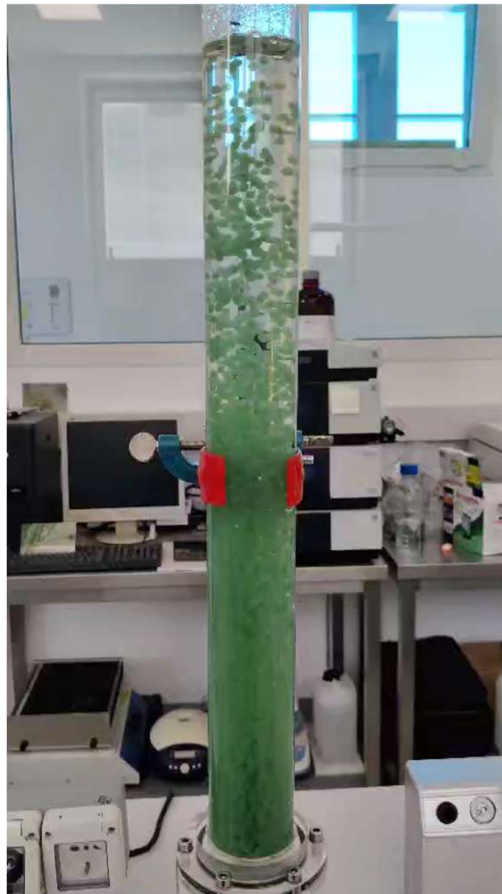
- **Characteristics of the reactor:**
  - **Height:** 511 mm
  - **Diameter:** 44 mm
  - **Inlet:** 9-10 mm
- **Gas flow rate:** between 600 and 750 ml/min
- **Solid phase dimension:** 5 mm
- **Inlet pore dimension:** 20  $\mu\text{m}$
- **Mesh quality:** 2 mm





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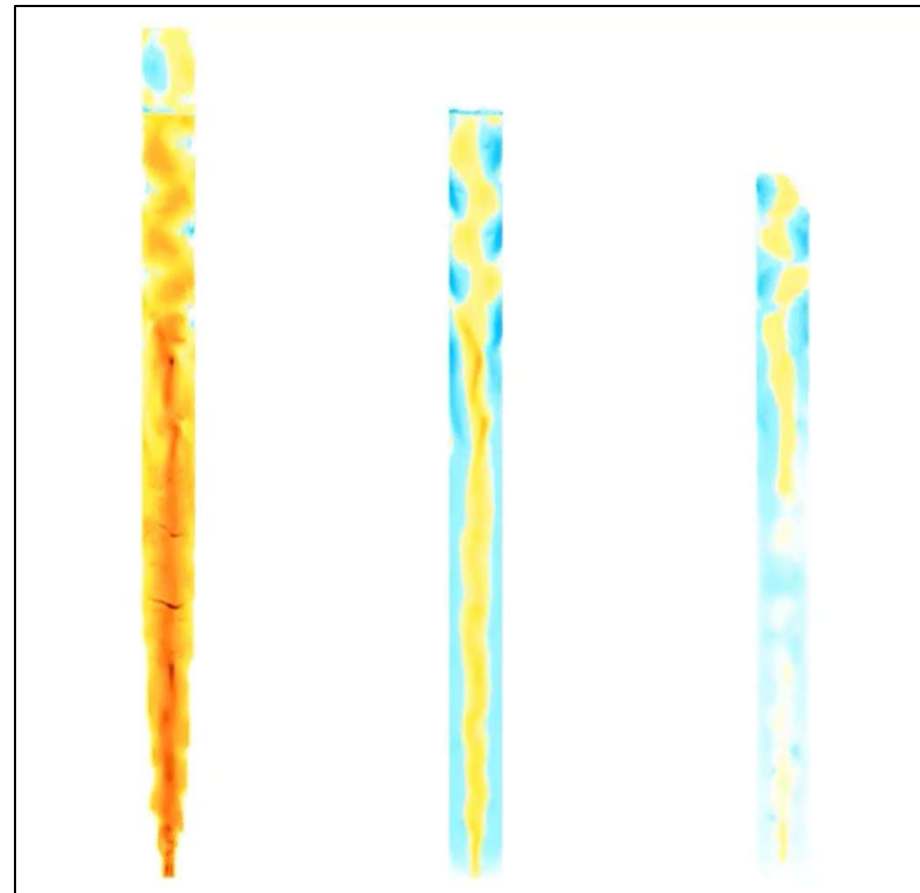
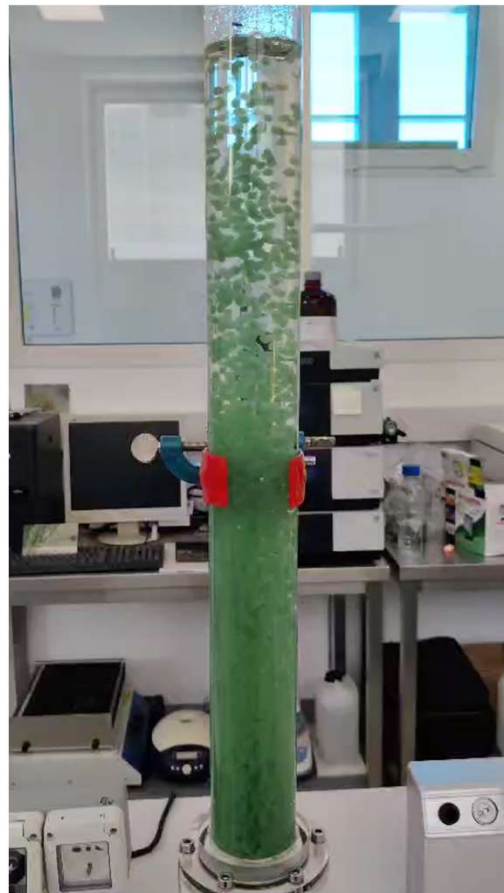


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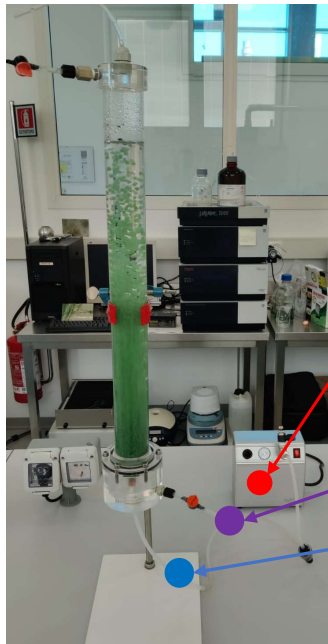


Gas

Water

Particles

- **Research and selection of suitable equipment**



### Bioreactor needs

- 0,5 l/min minimum
- 0,5 bar minimum



### Air compressor

- Max flow rate 10 l/min
- Max pressure 5,5 bar



### Pneumatic regulator

- Min exit pressure: 0,2 bar
- Max exit pressure: 4 bar
- Consumes around 4 l/min of air to work

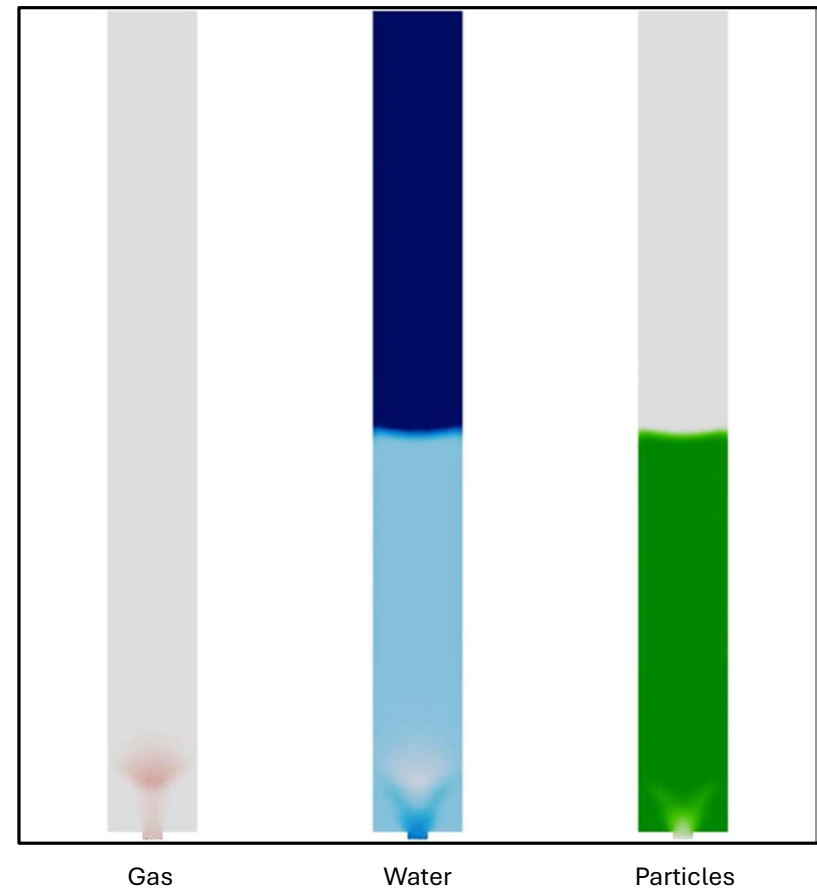
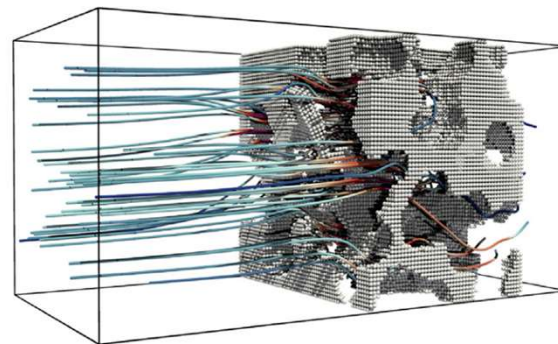
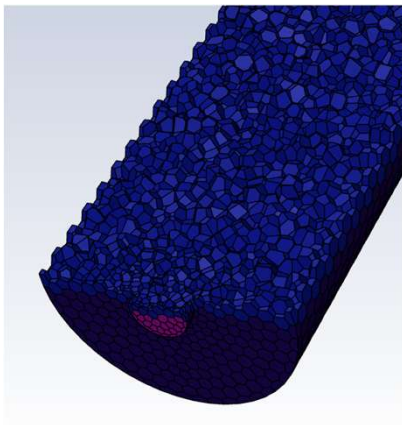


### Flow rate regulator

- Max op pressure: 7,5 bar
- Flow rate: between 0.2 and 10 l/min
- Consumes around 1 l/min of air to work



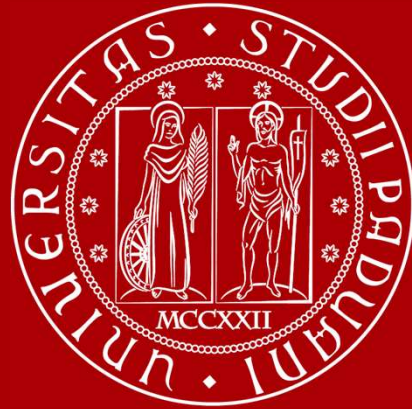
- **Data collection** with current experimental set and **comparison**
- **New experimental set up** and comparison
- **Completion of 2D versions** of all existent reactors
- Upgrade to **3D simulations**
- Reduced gravity
- Microscopic model state of the art



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Thanks for the attention



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